

***BNR to
Enhanced
Nutrient
Removal***

Maryland Center for Environmental Training

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www.mcet.org

BNR to Enhanced Nutrient Removal

7 Contact Hours

9 CC10 Hours

Upgrading sewage treatment plants for nutrient removal is one of Maryland's top environmental priorities. This course addresses the implications of upgrading from Biological Nutrient Removal (BNR) to Enhanced Nutrient Removal (ENR). Topics covered will include: a review of the basics of nitrification, denitrification, and phosphorus removal; various process configurations will be discussed to accomplish the required levels of nutrient removal; and process control testing and adjustments will also be examined to optimize ENR plant performance.

1. To discuss Biological Nutrient Removal (BNR) and Enhanced Nutrient Removal (ENR) options
2. To distinguish Biological Nutrient Removal (BNR) process trains from Enhanced Nutrient Removal (ENR) process trains
3. To discuss the evolution of Biological Nutrient Removal (BNR) processes to Enhanced Nutrient Removal (ENR) processes
4. To stress the effects that nutrient effluent requirements have on treatment options and costs
5. To share nutrient removal applications and ideas

Agenda

Morning

A. Introduction - Overview

- Nutrients – Phosphorus and Nitrogen
- Why remove nutrients?
- Conditions in the Chesapeake Bay
 - ✓ Submerged aquatic vegetation (SAV)
 - ✓ Loadings – phosphorus, nitrogen, and sediments

B. Nutrient Removal Options

- Phosphorus
 - ✓ Forms, sources, and typical concentrations
 - ✓ Chemical precipitation
 - ✓ Biological uptake
- Nitrogen
 - ✓ Forms (Nitrogen Cycle), sources, and typical concentrations
 - ✓ Nitrification
 - ✓ Denitrification
- Biological Nutrient Removal (BNR)
 - ✓ TN requirement < 8.0 mg/l
 - ✓ With and without carbon (Methanol) addition
- Enhanced Nutrient Removal (ENR)
 - ✓ TN requirement < 3.0 mg/l
 - ✓ With carbon addition
 - ✓ With tertiary treatment options

C. Evolution of BNR to ENR

- TN effluent requirement from < 8.0 mg/l to < 3.0 mg/l
- Nutrient loadings to the Bay still unacceptable

- Chemical addition for Phosphorus removal to < 0.3 mg/l is achievable
- New technologies are available to achieve TN limit of < 3.0 mg/l

Afternoon

D. Phosphorus Removal Options

- Chemical precipitation
 - ✓ Aluminum salts
 - ✓ Iron salts
- Biological uptake in both BNR and ENR options
 - ✓ Anaerobic zone for Phosphorus release
 - ✓ Aerobic zone for Phosphorus uptake
- Maximize biological uptake where possible to minimize costs for chemicals and related chemical sludge disposal
- Limit of Technology – 0.05 mg/l
- Anticipated permit levels – 0.1 mg/l to 0.3 mg/l

E. Biological Nutrient Removal Options

- TN requirement < 8.0 mg/l
- Typically, three stage, anaerobic, anoxic, aerobic processes installed
 - ✓ Phosphorus release
 - ✓ Denitrification
 - ✓ Nitrification
 - ✓ Phosphorus uptake
- Common BNR processes:
 - ✓ Ludzak-Ettinger - Three stage
 - ✓ A₂O – three stage
 - ✓ Bardenpho
 - Three stage
 - Modified five stage
 - ✓ University of Cape Town (UCT)
 - Three stage
 - Modified four stage
 - ✓ Virginia Initiative Project (VIP)
- Suspended growth, fixed film, oxidation ditch, and batch reactor designs have been used
- With and without carbon addition
- Limit of Technology – 5.0 mg/l
- Anticipated permit levels – 6.0 mg/l to 8.0 mg/l

F. Enhanced Nutrient Removal Options

- TN requirement < 3.0 mg/l
- Anaerobic, anoxic, aerobic process train usually installed with additional denitrification capability
 - ✓ Phosphorus release
 - ✓ Denitrification
 - ✓ Nitrification
 - ✓ Tertiary denitrification
 - ✓ Phosphorus uptake

- Common ENR processes:
 - ✓ Bardenpho – modified five stage
 - ✓ University of Cape Town (UCT) – modified four stage
 - ✓ Alterations/add-on options to BNR processes:
 - Integrated Fixed-Film Activated Sludge (IFAS) Hybrid Systems (e.g., rope media, sponge media, or web media)
 - High-rate Denitrification Biofilters (e.g., Tetra's CoLox System)
 - Moving Bed Biofilm Reactors (MBBR) using plastic elements w/o return sludge (e.g., AnoxKaldnes)
 - Membrane Filters (Zenon)
 - With carbon addition
 - Limit of Technology – 1.5 mg/l to 2.0 mg/l (Depends on Organic Nitrogen concentration)
 - Anticipated permit levels – 3.0 mg/l
- G. Regulations, Tributary Strategies, and the Chesapeake Bay

BNR and ENR



Presented by
Bill Shreve

Maryland Center for Environmental Training
College of Southern Maryland
La Plata, MD

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Introduction

Administrative

https://en.wikipedia.org/wiki/List_of_abbreviations_used_in_sanitation

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Process Training Sessions

Before class starts, please:

- Check in



During classes, please:

- Asks questions
- Feel free to get up at any time (i.e., rest rooms, phone calls, etc.)
- Answer questions on class evaluation and post quiz



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Housekeeping



- Start class – 8:00 am
- 10-minute Breaks – every hour
- Lunch – 1 hour, 11:30 am to 12:30 pm
- End class ~ 3:00 to 3:30 pm

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Ice Breaker

• Before we start, let's...

- Name one thing you know or want to know about:
 - Biological Nutrient Removal (BNR)
 - Enhanced Nutrient Removal (ENR)
 - “Biological Reactor Basins (BRB)” 1 – 5
 - “Biological Reactor Basin (BRB)” 6

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Instructor Expectations



- Begin and end class on time
- Be interactive
- Share experiences and needs
- ***Make this an enjoyable and informative experience!***

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Groundrules

- Participate at your own comfort level
- Use terms we all understand
- Everyone is different, so please show respect for others
- Listen with an open mind
- Express opinions
- Maintain confidences



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Introduction

Definitions and Acronyms

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Acronyms

- BNR – Biological Nutrient Removal
- ENR – Enhanced Nutrient Removal
- CBP – Chesapeake Bay Program
- TMDL – Total Maximum Daily Loading
- WLA – Waste Load Allocation
- MLE – Modified Ludzack-Ettinger Process (BNR)
- EMLE- Enhanced Modified Ludzack Process (ENR)
- SBR – Sequencing Batch Reactor
- MBBR – Mixed Bed Bioreactor
- COMAMMOX – COMPlete AMMOnia OXidation
- ANAMMOX – ANaerobic AMMOnia OXidation

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Nutrients

- TN – Total Nitrogen
 - Soluble and particulate
 - Organic nitrogen - N_{org}
 - NH_3 – Ammonia
 - NO_2 – Nitrite
 - NO_3 – Nitrate
- TP – Total Phosphorus
 - Soluble and particulate
 - PO_4 – Ortho-phosphorus
 - Organic
 - Polyphosphates

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Nutrients

- TN – Total Nitrogen ($N_{org} + NH_3 + NO_3 + NO_2$)
- TP – Total Phosphorus ($PO_4 + P_{org} + P_{poly}$)

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Microorganisms

- **Aerobic** (Oxic) - Organisms requiring, or not destroyed, by the presence of free oxygen
- **Anoxic**: Organisms requiring, or not destroyed, by the absence of free oxygen; nitrates (NO_3) are present.
- **Anaerobic** - Organisms requiring, or not destroyed, by the absence of free oxygen and NO_3
- **Facultative** - Organisms able to function both in the presence or absence of free oxygen
- **Heterotrophic** - Organisms that use organic materials as their source of cell carbon
- **Autotrophic** - Organisms able to use carbon dioxide and other inorganic matter as their source of carbon
- **Filamentous** – Bulking organisms that grow in thread or filamentous form

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Introduction

Objectives, Focus, and Agenda

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Learning Objectives

- **Objective 1** - To discuss the Chesapeake Bay restoration efforts and regulatory “drivers” for BNR and ENR
 - Bay conditions in the 1970s and early 1980s
 - 1987 Bay Agreement (Begin using BNR)
 - 2000 Bay Agreement (Begin using ENR)
 - 2010 TMDL (Imposed by EPA)
- **Objective 2** - To discuss methods for nitrogen and phosphorus removal
- **Objective 3** - To discuss the evolution of BNR technologies to ENR

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Participant Focus

- What information can you use at your work location?
 - ENR fundamentals
 - Troubleshooting ENR processes
 - Meeting nutrient discharge standards
- What information can you contribute to the discussion?
 - ENR experiences and practices
 - Step feed ENR issues

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OUTLINE

- Water quality in the Chesapeake Bay
 - 1970s and early 1980s condition
 - Need for 40 percent reduction in nutrient loadings to restore Bay conditions
- Regulatory Background
 - 1987 and 2000 Bay Agreements
 - 2010 Agreement - TMDL (EPA)
- BNR and ENR configurations – Overview
- BNR configurations
- ENR configurations
- Summary

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Expected Learning Outcomes

Participants will be able to:

- Discuss the regulatory framework for nutrient removal in the Chesapeake Bay watershed
- Discuss major BNR processes
- Discuss major ENR processes
- Discuss options to upgrade BNR facilities to ENR
- Discuss process control options
- Discuss trouble-shooting options

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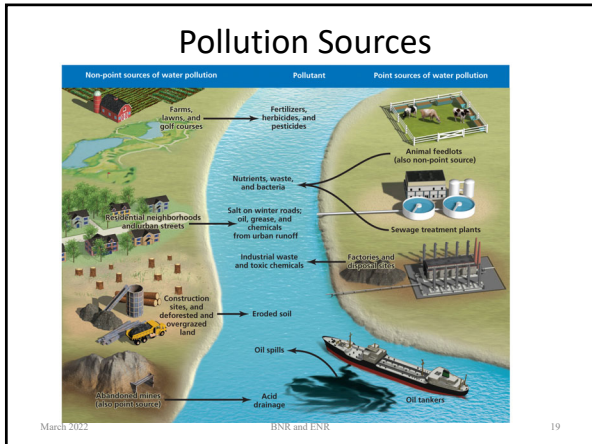
Chesapeake Bay

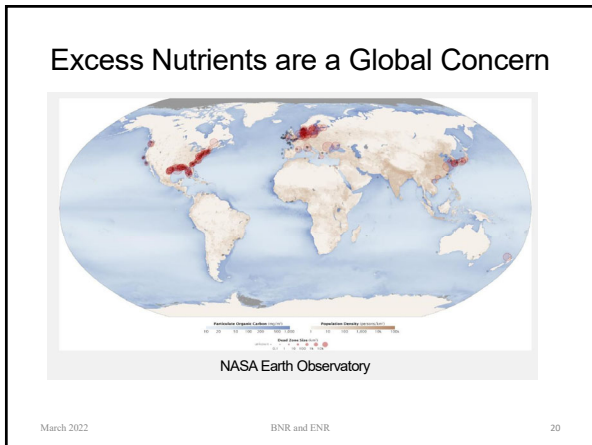
Bay Health and Regulations

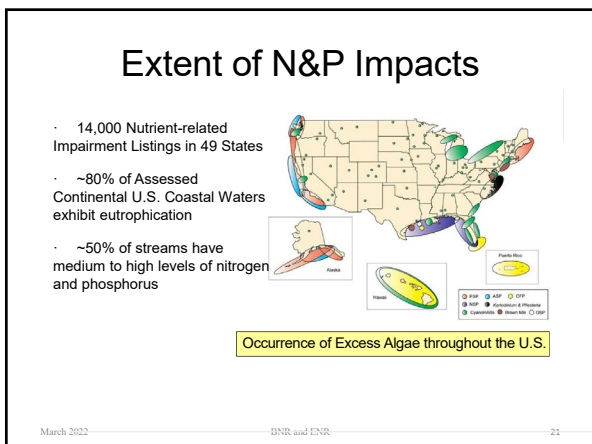
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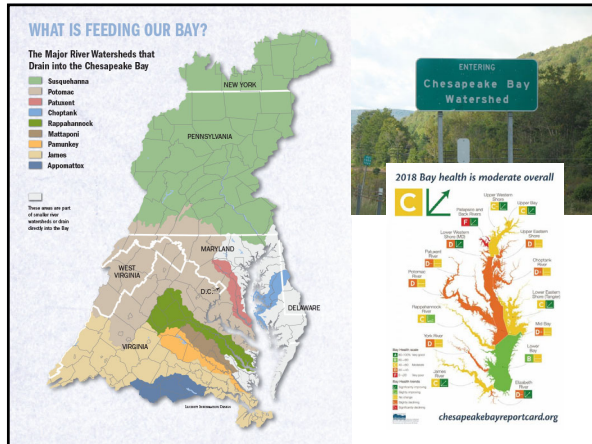
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Water Quality Conditions

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**University of Maryland
Center for Environmental Science**

- “Bay Health” Annual Reports (Since 2007)
- Bay health affected by elevated nutrient and sediment loads, which results in water quality and biotic (biological) degradation

Aquaculture and Restoration Ecology Laboratory at Horn Point Laboratory, Cambridge, Maryland; Photo by Kirsten Frese

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Chesapeake Bay Health

- Bay Health - progress of six indicators towards established ecological thresholds.
- Water quality indicators/Index (WQI) are:
 - Chlorophyll *a*
 - Dissolved oxygen
 - Water clarity
- Biotic indicators/Index (BI) are:
 - Submerged aquatic vegetation (SAV)
 - Benthic Index of Biotic Integrity
 - Phytoplankton Index of Biotic Integrity

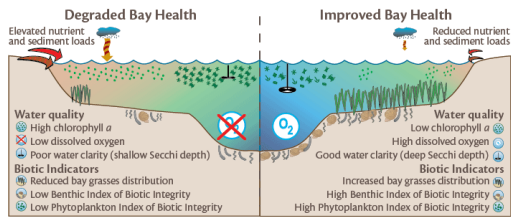
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Chesapeake Bay Health

- Bay Health Index (BHI) - average of Water Quality Index (WQI) and Biotic Index (BI) scores for each reporting region



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Key Water Quality Indicators

- Chlorophyll *a*
- SAV – Submerged aquatic vegetation
- Dissolved Oxygen
- All three are showing degrading trends

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The Chesapeake Bay Program

- In the late 1970s, a rapid loss of aquatic life was reported in a 5-year study of Bay conditions
- The study identified excess nutrient pollution as the main source of the Bay's degradation
 - Ammonia toxicity also contributed to degradation
 - Loss of submerged aquatic grasses was key observation

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Submerged Aquatic Vegetation

- SAV areas are important habitats for fish and molting crabs
- SAV contributes to the reduction of shoreline erosion and the trapping of sediments and nutrients from overlying waters, which leads to improved water quality and clarity
- A decline in SAV populations began in the 1960s and became a problem in the 1970s

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Submerged Aquatic Vegetation

- SAV is rooted vegetation that grows under water in shallow zones where light penetrates



Wild celery
Upper Bay



Redhead grass
Mid-Bay

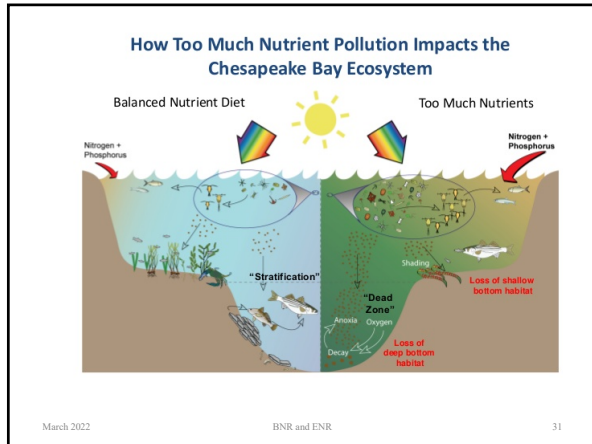


Eel grass
Lower Bay

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Development of Chesapeake Watershed Models

Model Revision	Characteristics		Advances	Simulation Period	Decisions Supported
	Watershed	Bay			
Phase I (1985)	5 land uses; 64 segments	Steady state	First coupling of watershed, hydrodynamic, and water quality models	Summer data - 1965, 1984, and 1985	General goal of 40% reductions of controllable loads (CBP, 1987)
Phase 2 (1992)	Expanded agriculture simulation detail	Dynamic 4,000 grid cells	Integrated sediment flux model; included atmospheric deposition	4 continuous years (1984 – 1987), hourly time intervals	Nutrient load reductions to achieve CBP (1987) allocation goals
Phase 4.3 (2003)	9 land uses; 94 segments	Dynamic 13,000 grid cells	Integrated simulation of land and soil contaminant runoff processes; included SAV and benthic deposit models	14 continuous years (1985 – 1994)	Nutrient load allocations
Phase 5.3 (2010)	25 land uses; 899 segments	Dynamic 57,000 grid cells	Enhanced segmentation, land uses, and mechanistic detail	21 continuous years (1985 – 2005)	TMDL

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Chesapeake Bay Program

- Bay degradation findings led to the formation of the Chesapeake Bay Program in 1983 as a governance means to restore water quality in the Bay

Chesapeake Bay Program
Science. Restoration. Partnership.

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Chesapeake Bay Program

- The Chesapeake Bay Program includes:
 - Signers of the original 1983 Bay Agreement:
 - Maryland
 - Virginia
 - Pennsylvania
 - The District of Columbia
 - EPA - sets Chesapeake Bay water quality limits
 - The U.S. Department of Agriculture
 - Headwater jurisdictions:
 - Delaware
 - New York
 - West Virginia

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Chesapeake Bay Program

- The Program is led by the Chesapeake Executive Council, which includes:
 - The EPA Administrator
 - Governors of Maryland, Pennsylvania, and Virginia
 - The mayor of the District of Columbia



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Chesapeake Bay Program

- CBP Agriculture and Wastewater Workgroups
 - Model Bay watershed improvements (since 1985)
- Water quality restoration efforts:
 - Implementing pollution reduction practices on urban and suburban lands
 - Reducing air pollution deposited in the watershed

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1987 Chesapeake Bay Agreement

- In a 1987 Chesapeake Bay Agreement:
 - Nutrient water quality targets for 2000 were set (40% less than 1985 conditions)
 - USEPA, MD, VA, DC, PA and the Chesapeake Bay Commission – Signatories to agreement
 - USEPA has the lead on setting water quality standards for the Bay:
 - Based on water quality needs
 - Based on nutrient removal technology available

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2000 Chesapeake Bay Agreement

- In a 2000 Chesapeake Bay Agreement:
 - The 40 percent reduction goal would continue beyond 2000 to 2010
 - Signatories would include Delaware, New York, and West Virginia
 - States and DC began planning for nutrient removal at their source – tributary strategies

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Total Maximum Daily Load (TMDL)

- In December 2010, EPA established Total Maximum Daily Loads (TMDL) for the Bay watershed
- The 2010 Bay TMDL was prompted by insufficient progress and continued poor water quality in the Chesapeake Bay and its tidal tributaries
- Nutrient load allocations (million pounds/year):

	<u>2000</u>	<u>2010 TMDL</u>
Nitrogen	175	186
Phosphorus	12.8	12.5

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2010 Chesapeake Bay Agreement

- In a 2010 Chesapeake Bay Watershed Agreement:
 - States and DC committed to meet sector reduction goals
 - Total Maximum Daily Load, or TMDL
 - Waste Load Allocation, or WLA
 - The 40 percent nutrient removal reduction goal would continue beyond 2010 to 2025
 - EPA would review progress by 2017

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Total Maximum Daily Load (TMDL)

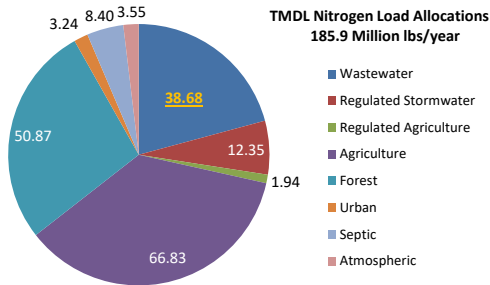
- TMDL pollution limits are designed to ensure:
 - Restoration of the Bay and its tidal rivers by 2025
 - Best Management Practices (BMPs) in place by 2017 to meet 60 percent of pollution reductions
- Annual TMDL Bay watershed limits:
 - 185.9 million pounds of nitrogen (excludes tidal water atmospheric deposition of nitrogen)
 - 12.5 million pounds of phosphorus
 - 6.45 billion pounds of sediment

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TMDL Nitrogen Load Allocations

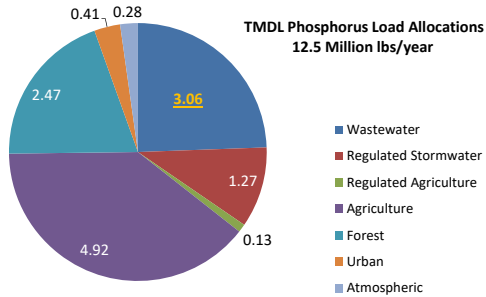


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TMDL Phosphorus Load Allocations



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Wastewater Sector Waste Load Allocations

- Nitrogen: 38.7 million pounds/year
- Phosphorus: 3.06 million pounds/year
- Interim target date: 2017 for 60% reductions (from 2010)
- Target date: 2025 for achieving WLAs

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Total Maximum Daily Load (TMDL),

- Progress in implementing the Bay Total Maximum Daily Load (TMDL) is tracked by the CBP's "ChesapeakeStat"
- Elements of a TMDL:
 - "Waste load allocations" for point sources
 - Sewage treatment plants
 - Regulated urban stormwater systems
 - Regulated animal feeding operations
 - "Load allocations" for non-point sources
 - Runoff from agricultural lands
 - Non-regulated stormwater from urban/suburban lands

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Wastewater Nutrient Removal

- **Total Phosphorus (TP)** has been removed well in the past
 - Less than 0.3 mg/l TP; even less than 0.1 mg/l
 - **Bay 2010 TMDL Target: Less than 0.3 mg/l TP**
 - Low threshold - Limit of Technology /State of the Art (LOT/SOA) is less than 0.05 mg/l TP (soluble Org-P)
 - TMDL – Total maximum daily loading

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Nutrient Removal

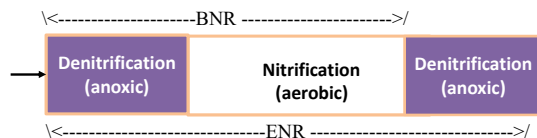
Nutrient	Removal Process
• Nitrogen	<ul style="list-style-type: none"> • Nitrification <ul style="list-style-type: none"> – Ammonia Conversion – $\text{NH}_3\text{-N}$ to $\text{NO}_3\text{-N}$ – Oxygen and alkalinity needed • Denitrification <ul style="list-style-type: none"> – Nitrate Removal – $\text{NO}_3\text{-N}$ to Nitrogen gas (N_2) – Carbon source needed
• Phosphorus	<ul style="list-style-type: none"> • Biological Uptake <ul style="list-style-type: none"> – Conventional – Excess • Chemical Precipitation

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Common BNR/ENR Configurations



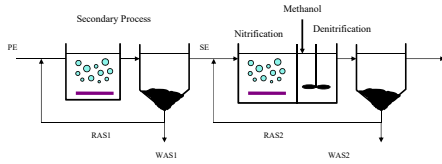
- BNR:
 - Modified Ludzack-Ettinger (MLE)
 - Anaerobic/Anoxic/Oxic (A2O)
 - University of Cape Town Process (UCT)
- ENR:
 - Enhanced MLE/4-stage Bardenpho
 - MLE with Denitrification Filter

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Two Sludge System for BOD and Nitrogen Removal



Example: Blue Plains, DC Water 370 MGD

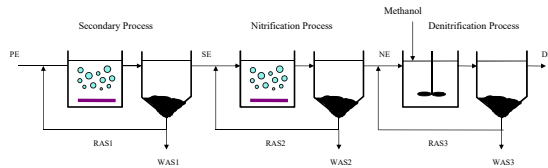
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Three Stage System for BOD and Nitrogen Removal

Post Denitrification w/Methanol



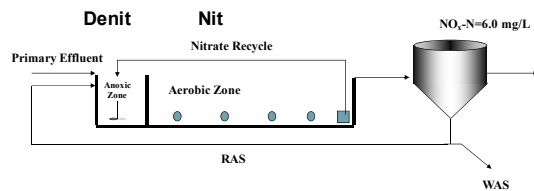
Example: Western Branch WWTP, WSSC 30 MGD

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Basic BNR Process



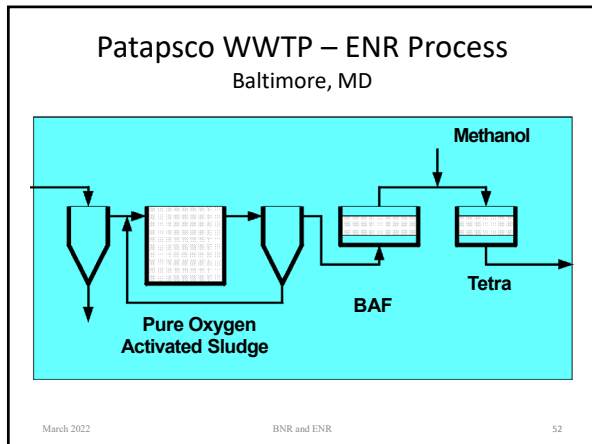
Nitrogen removal:

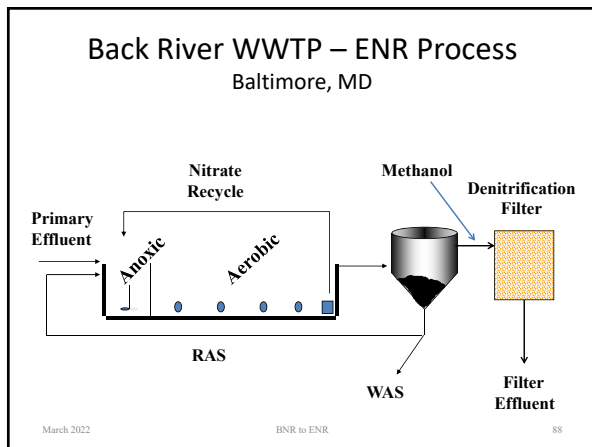
- Basic biological denitrification-nitrification process
- Complete denitrification is not possible

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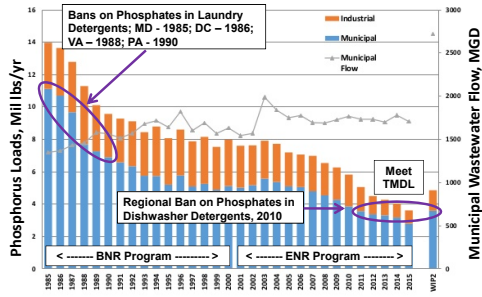
Nutrient Removal

FORM	Removal Mechanism	LOT ¹ , mg/L
TN		< 1.5
NH ₃ -N	Nitrification	< 0.1
NO ₃ -N	Denitrification	< 0.1
Org-N:		
Particulate	Solids Separation	< 0.5
Soluble	Ammonification	0.5 – 1.0
TP		< 0.05
Particulate	Solids Separation	< 0.05
Soluble	Biological uptake and chemical precipitation	< 0.05

¹ LOT – Limit of Technology

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TP Loadings to the Chesapeake Bay - Wastewater



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Wastewater Discharge Limits

Typical Total Phosphorus Standards, mg/l

- Moderate 0.5 - 1.0 (BNR)
 - **Bay Target < 0.3 (ENR)**
 - **Potomac River < 0.18 (ENR)**
 - Very Severe < 0.1
 - LOT/SOA(a) < 0.05
- (a) Limit of Technology/State of the Art

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Wastewater Nutrient Removal

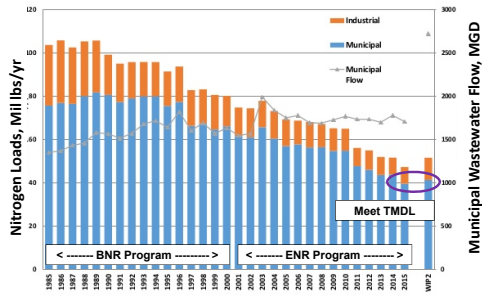
- Enhanced (ENR) Total Nitrogen (TN) removal is now required:
 - Current 3 to 5 mg/L of TN is not adequate (BNR)
 - **Bay 2010 TMDL Target: Less than 3.0 mg/l TN**
 - Low threshold - Limit of Technology /State of the Art (LOT/SOA) is about 1.0 mg/l TN (soluble Org-N)
 - TMDL – Total maximum daily loading

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TN Loadings to the Chesapeake Bay - Wastewater



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Wastewater Sector

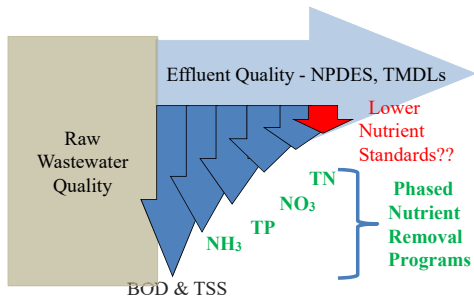
- Wastewater sector nutrient removal goals were met in 2015 because of:
 - BNR upgrades from 1985 – 2000
 - ENR upgrades from 2000 – 2015
- In 2016, EPA announced the wastewater sector’s 2025 nutrient removal goals had been effectively met a decade early...!

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Future - Role and Impact of Nutrients



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How will future regulations affect Nutrient Removal Requirements?

Regulatory Challenges:

- Clean Water Act
- Chesapeake Bay Program Regulations
- State Regulations
 - Follow EPA lead
 - Nutrients
 - Sludge
- Local Ordinances



Nutrient Removal

Overview

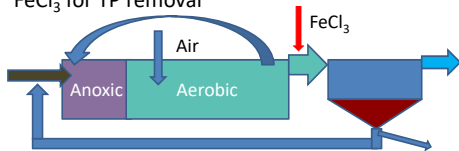
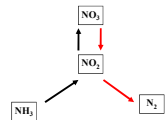
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Nutrient Removal

- Nitrification (*Nitrosomonas* and *Nitrobacter*)
 $NH_3 + O_2 \rightarrow NO_2^- \rightarrow NO_3^-$
- Denitrification
 $NO_3^- + \text{organics} \rightarrow CO_2 + N_2$
- Process adaptation – MLE
- $FeCl_3$ for TP removal



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Nutrient Removal

- **Why remove Nutrients (nitrogen and phosphorus):**
 - Nutrients contribute to algae growth
 - Excess algae growth (Eutrophication) causes water quality issues:
 - Loss of water clarity
 - Limitation on sunlight penetration
 - Oxygen depletion
 - Fish and marine life die-off
 - Submerged aquatic vegetation (SAV) die-off

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Historical Overview

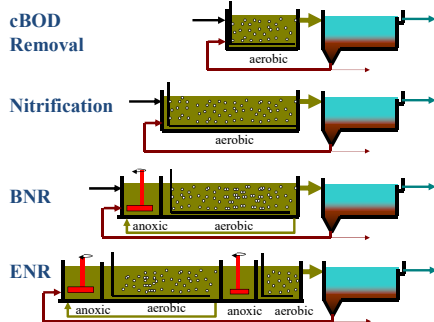
- 1920s - 1960s
 - cBOD Removal
 - Nitrification
- 1970s – Chemical addition for phosphorus removal
- 1980s to 2000 – BNR development and application
- Past 20 years – BNR to ENR

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Evolution of Activated Sludge



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Nutrient Removal

- | Nutrient | Removal Process |
|--------------|--|
| • Nitrogen | <ul style="list-style-type: none"> • Nitrification <ul style="list-style-type: none"> – Ammonia Conversion – $\text{NH}_3\text{-N}$ to $\text{NO}_3\text{-N}$ – Oxygen and alkalinity needed • Denitrification <ul style="list-style-type: none"> – Nitrate Removal – $\text{NO}_3\text{-N}$ to Nitrogen gas (N_2) – Carbon source needed |
| • Phosphorus | <ul style="list-style-type: none"> • Biological Uptake <ul style="list-style-type: none"> – Conventional – Excess • Chemical Precipitation |

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Nutrient Removal

FORM	Removal Mechanism	LOT ¹ , mg/L
TN		< 1.5
NH ₃ -N	Nitrification	< 0.1
NO ₃ -N	Denitrification	< 0.1
Org-N:		
Particulate	Solids Separation	< 0.5
Soluble	Ammonification	0.5 – 1.0
TP		< 0.05
Particulate	Solids Separation	< 0.05
Soluble	Biological uptake and chemical precipitation	< 0.05

¹ LOT – Limit of Technology

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Meeting Nutrient Discharge Limits Process Strategies

1. **Multiple barriers for TN removal**
 - Pre-anoxic zone (first stage denitrification)
 - Nitrification – aerobic zone
 - IFAS (enhanced nitrification, optional)
 - Post anoxic zone (second stage denitrification)
 - Denitrification filters (in lieu of post anoxic zone)
2. **Multiple barriers for TP removal**
 - Biological uptake
 - One (maybe two) chemical application points
 - Filtration for TSS (particulate TP) removal

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Nutrient Removal


Nitrogen

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Forms of Nitrogen

Organic Nitrogen

- Complex Compounds
- Protein (plant & animal)
- Amino Acids
- etc.



Oxygen Demand
Nutrient Source

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Forms of Nitrogen

Ammonia – NH₃


Toxic
Oxygen Demand

Nitrite – NO₂⁻


Chlorine Demand

Nitrate – NO₃⁻

Health Concern



All Are
Nutrients
(fertilizer)



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Forms of Nitrogen

FORM	REMOVAL PROCESS
<ul style="list-style-type: none"> Organic-N 	<ul style="list-style-type: none"> Converts to ammonia; a small soluble portion is non-reactive (1.0 mg/l)
<ul style="list-style-type: none"> Ammonia(um) ($\text{NH}_3/\text{NH}_4^+$) 	<ul style="list-style-type: none"> Most abundant form; converts to nitrites/nitrates under aerobic conditions (nitrification)
<ul style="list-style-type: none"> Nitrite (NO_2^-)/Nitrate (NO_3^-) 	<ul style="list-style-type: none"> Converts to N_2 under anoxic (no oxygen) conditions (denitrification)

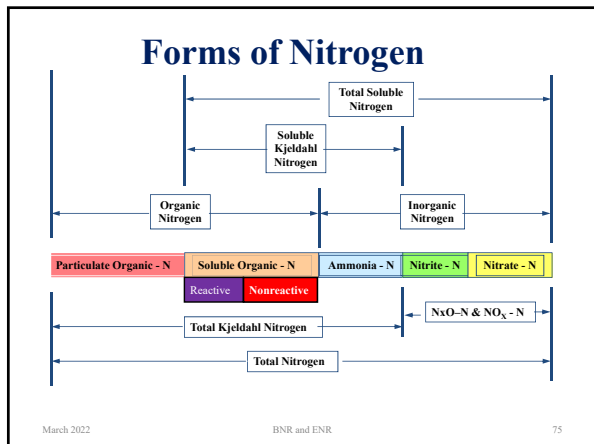
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Forms of Nitrogen

<ul style="list-style-type: none"> Ammonia(um) ($\text{NH}_3/\text{NH}_4^+$) Organic Nitrogen (Org-N) 	}	TKN (Un-oxidized)
<ul style="list-style-type: none"> Nitrite (NO_2^-) Nitrate (NO_3^-) 	}	NO_x (Oxidized)

Total Nitrogen (TN) = TKN + NO_x
TKN = Total Kjeldahl Nitrogen

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Background Uptake

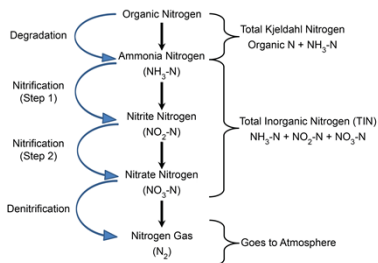
- Physical removal of particulate organic nitrogen
- Conventional biological assimilation of NH_3
 - To satisfy biological needs
- Nitrification/Denitrification
 - Aerobic zones
 - Anoxic zones

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Nitrogen Cycle in Nature

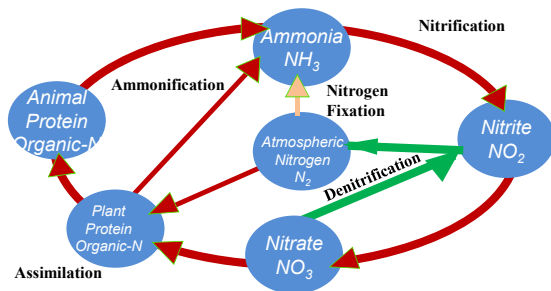


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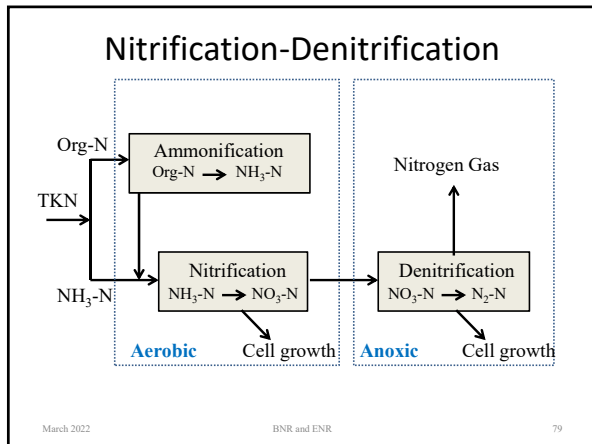
Simplified Nitrogen Cycle in Nature

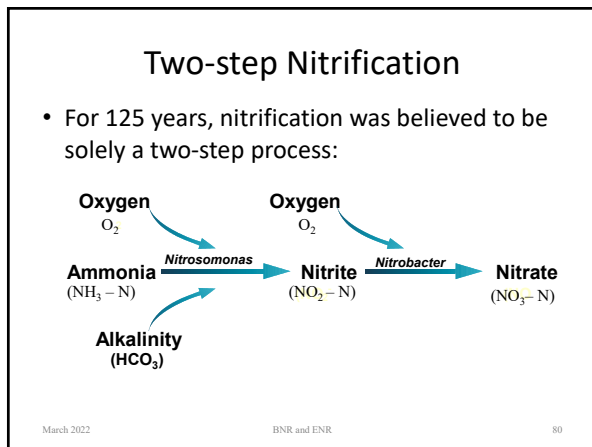


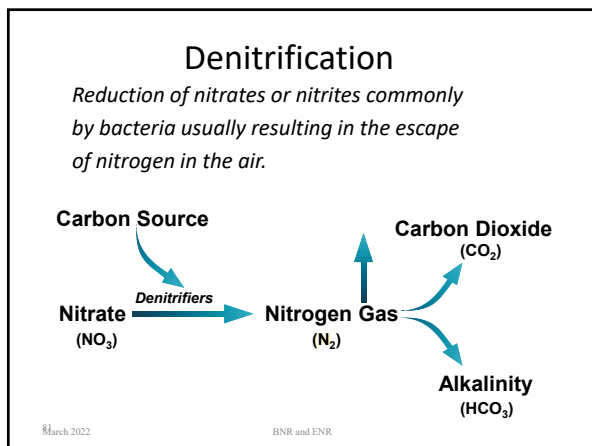
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Two-step Nitrification

- Two-step nitrification depends on two organisms, *Nitrosomonas* and *Nitrobacter* which was the basis for hundreds of studies on nitrification in wastewater treatment
- A single microbe capable of catalyzing both nitrification steps may actually conserve energy

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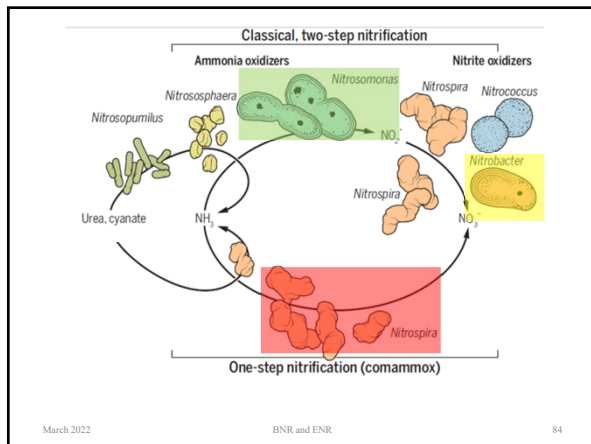
Nitrification



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One-step Nitrification - Comammox

- **Comammox** (COMplete AMMonia Oxidixer) is the name for a single organism that can convert ammonia into nitrite then nitrate
- Existence of comammox bacteria were first predicted in 2006
- In 2015, *Nitrospira* bacteria were confirmed as comammox organisms in nitrification
- The Nitrogen cycle has since been updated...!

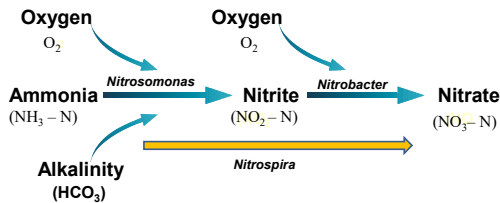
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Nitrification

The oxidation (as by bacteria) of ammonia and organic nitrogen to nitrites (NO_2^-) and then further oxidation of nitrites to nitrates (NO_3^-).

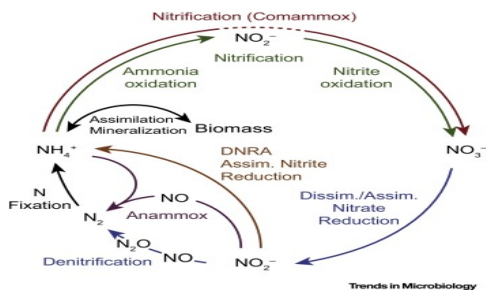


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Nitrogen Cycle in Wastewater (2016)



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Nitrification Process Monitoring

- Oxygen requirements:
 - 4.6 mg/mg NH₃-N converted
 - Maintain DO in process between 2.0 – 4.0 mg/l
- Alkalinity requirements:
 - 7.1 mg/mg NH₃-N converted
 - Maintain alkalinity >70 mg/l CaCO₃

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Nitrification

***Heterotrophic** Bacteria Break Down Organics
Generate NH₃, CO₂, and H₂O

***Autotrophic** Bacteria Utilize Inorganic Compounds
(and CO₂ as a Carbon Source)

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Nitrification

Nitrification of Ammonia Occurs in
Two Steps

***Autotrophic** Bacteria Utilize Inorganic Compounds
(and CO₂ as a Carbon Source)



Nitrosomonas



Nitrobacter

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Operational Controls for Nitrification

Air Requirements

1.5 lbs O₂ / lb BOD

4.6 lbs O₂ / lb TKN

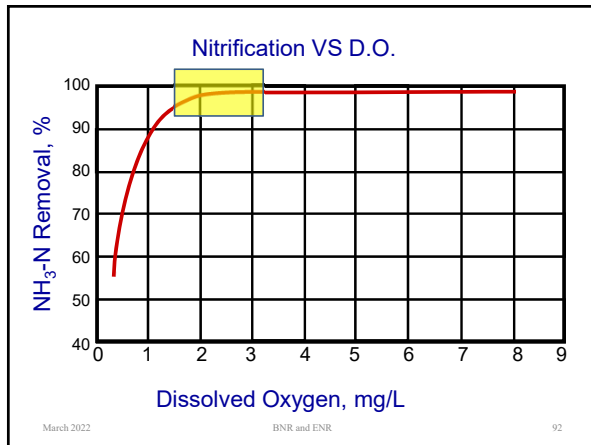
Minimum D.O. in Aeration Tank

2 - 3 mg/L

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Nitrification Process Monitoring

- Key Factors:
 - Slow growth requires adequate **aerobic SRT**
 - DO** typically >2mg/L
 - pH** 6.5-7.5
 - Target effluent alkalinity of 50 to 75 mg/L as CaCO₃
- Overall Reaction:
 - $\text{NH}_4^+ + 2 \text{O}_2 \rightarrow \text{NO}_3^- + 2\text{H}^+ + \text{H}_2\text{O}$

Temperature (°C)	Minimum Aerobic SRT (days)
10	7.5
15	4.5
20	2.5
25	1.5
30	1.0

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Nitrification Control Parameters

Temperature

- Nitrifiers lose about ½ their activity for each 10°C temperature drop
- In winter, put additional aeration tanks on line, or increase MLSS
- Either action will increase MCRT

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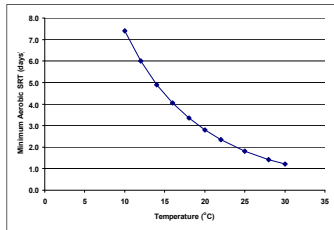
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Nitrification Process Monitoring

▪ Key Factor 1

- Slow growth requires adequate aerobic SRT
- **MAINTAIN ADEQUATE SOLIDS INVENTORY**



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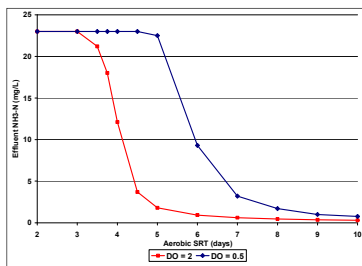
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Nitrification Process Monitoring

▪ Key Factor 2

- Maintain target DO concentration



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Importance of Dissolved Oxygen

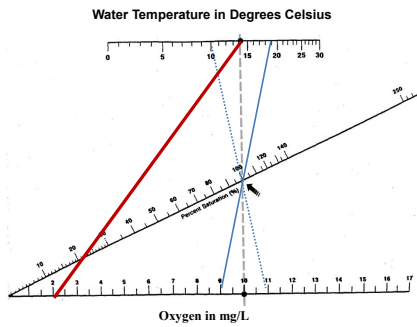
- Oxygen is sparingly soluble in water
- DO is a growth-limiting substrate
- *Critical oxygen concentration* is about 10% to 50% of DO saturation in water
 - 10% minimum saturation for BOD removal (> 1.0 mg/l DO)
 - 20% minimum saturation for ammonia conversion (> 2.0 mg/l DO)

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D.O. - Percent Saturation in Water



Source: Department of Fisheries and Aquatic Sciences, University of Florida

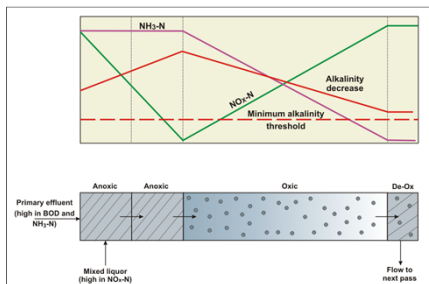
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Nitrification Process Monitoring

- **Key Factors – NH₃/NO₃, D.O., SRT, and Alkalinity**
 - Maintain target effluent NH₃/NO₃, DO, and alkalinity



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Nitrification Problems - Summary

Possible Causes	Solution
Insufficient MCRT (target – varies with temperature)	Increase MCRT to establish nitrification by reducing sludge wasting or increasing MLSS levels
Insufficient DO in aerator (target - 2.0 mg/l goal)	Increase aeration by adjusting air valves, increasing blower output, or turning on another blower.
Insufficient alkalinity (target – NLT 70 mg/l CaCO ₃)	Add supplemental alkalinity to maintain target CaCO ₃ concentrations in effluent
Chemical inhibition of nitrifiers	Trace source of improper discharge of nitrification inhibitors and eliminate at source

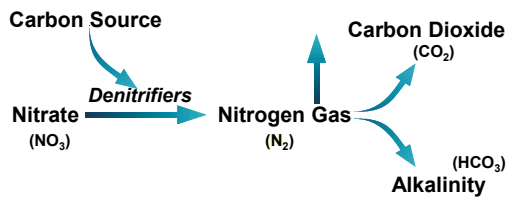
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Denitrification

Reduction of nitrates or nitrites commonly by bacteria usually resulting in the escape of nitrogen in the air.



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Denitrification

Note: (Almost) all nitrates returned to the pre-anoxic zones should be denitrified.

The “goal” NO₃-N concentration in the effluent from the last anoxic zone should be between 0 and 0.5 mg/L.

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Denitrification

- Requires three conditions:
 - Organic carbon must be available
 - DO concentrations must be low
 - HDT must be sufficient

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Conditions for Denitrification

No oxygen:

DO less than 0.2 mg/L

No aeration

Carbon source:

Primary Effluent

Endogenous

Methanol or other carbon source

Mixing:

Submersible mixers

Vertical mixers

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Denitrification

- Many different types of bacteria can denitrify
- The process requires organic carbon and produces 3.57 mg of alkalinity as CaCO_3 for every 1 mg/L nitrate ($\text{NO}_3\text{-N}$) denitrified
- Between 2.7 and 3.3 mg/L of methanol is needed for every 1 mg/L $\text{NO}_3\text{-N}$

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Denitrification

- **If effluent nitrate-nitrogen is above the goal:**

- Verify nitrate recycle pumps are running.
- Check nitrate recycle pump speed.
- Verify very low DO in the anoxic zones.
- Consider if low influent BOD or slowly degradable influent BOD could be inhibiting the process.

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Keys to Successful Nitrogen Removal

- **Nitrification**

- Adequate Aerobic SRT – **Keep Solids High!**
- Adequate D.O./oxygen transfer
- Adequate Alkalinity/pH

- **Denitrification**

- **Successful nitrification**
- Anoxic zones
- No D.O
- Carbon

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Inhibition of Denite Process

- Environmental Conditions

- pH
- Temperature
- **Aerobic Conditions! Keep DO < 0.2 mg/L**

- Insufficient amount of rbCOD (Carbon Substrate).

- Presence of Chemical Inhibitors:

- Substrates, intermediates, and products of denitrification
- Synthetic organic chemicals
- Heavy metals - Hg, Ni, Pb, etc.

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High DO in the Anoxic Zones

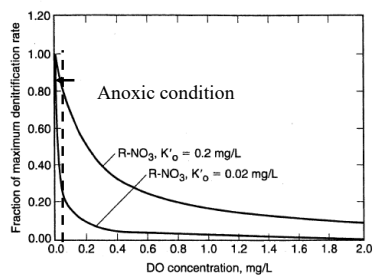
- High DO in the anoxic zones may be more of a problem during the winter because more DO can be absorbed by colder water and biological kinetics are reduced.
- Lower the nitrate recycle rate in the winter if necessary

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Reduction in rate of Denite as a function of D.O.
(K'_o is oxygen inhibition constant)



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Carbon for Denitrification

- Influent WW Carbon
 - Utilized in first anoxic zone
 - EBPR can compete for carbon
 - Limited carbon available for secondary anoxic zones – and effective denite
- Endogenous Carbon
 - Slow kinetics – limited denite in post-anoxic zones
- Supplemental Carbon
 - Methanol typically used
 - But requires methylotrophic population!
 - Alternatives to methanol – ethanol, acetic acid, glycerin, sugars, mono-propylene glycol, proprietary products

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Other Carbon Sources

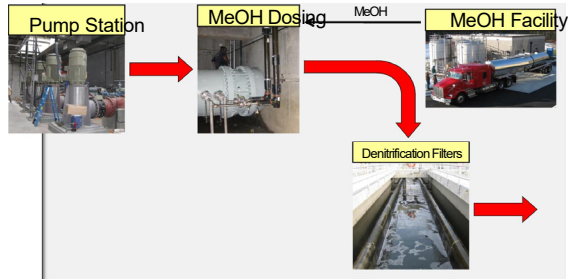
- Alcohols
 - Methanol
 - Ethanol
- Glycerol/glycerin – (Biodiesel by-products)
- Acetates - (Acetic acid, sodium acetate)
- Carbohydrates - (Sucrose, sugar water, corn syrup)
- MicroC™ – Carbohydrate (1000), glycerin (2000), alcohol based blends (3000)

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Let's Focus on Adding Supplemental Carbon



Jan 2019

Automation of BNR/ENR Processes

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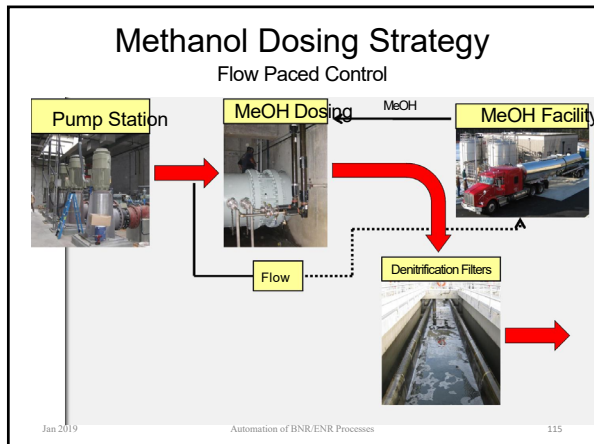
Adding Supplemental Carbon

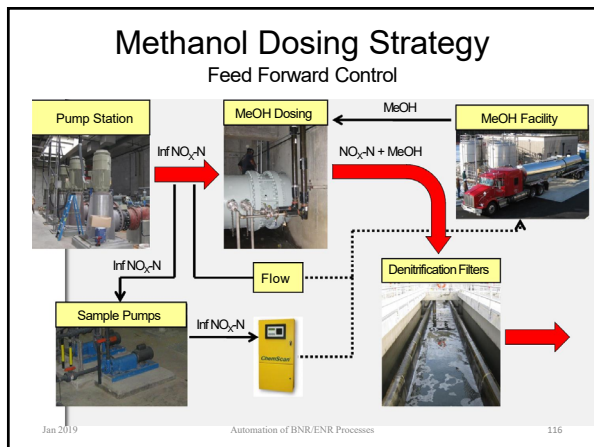
- Typical control modes for supplemental carbon addition:
 - **Manual mode** – operator sets feed rate
 - **Flow-paced** – feed forward control: dose determined by desired nitrate removal – feed rate based on flow
 - **Nutrient-paced** – dual point control: paced based on nitrate load into anoxic zone; speed adjusted based on effluent nitrate concentration

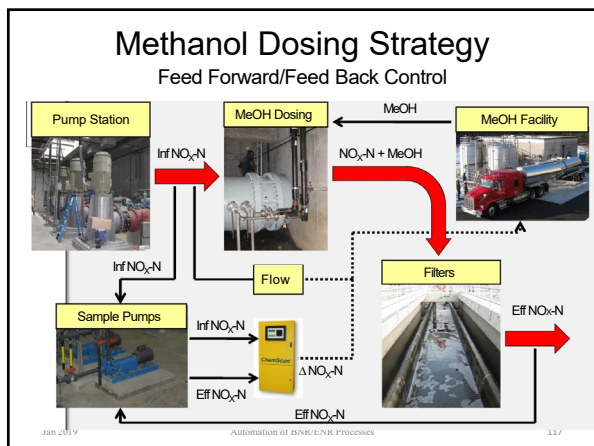
Jan 2019

Automation of BNR/ENR Processes

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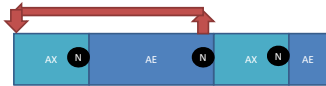






Adding Supplemental Carbon

- Nutrient-paced mode is the most accurate
 - Requires nitrate analyzers; locate in/out of anoxic zone and filters
 - With DO probe can account for DO entering the zone to improve results



Jan 2019

Automation of BNR/ENR Processes

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Nutrient Removal

Phosphorus

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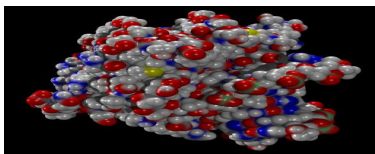
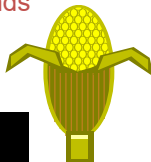
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Forms of Phosphorus

Organic Phosphorus

- Complex organic compounds
- Soluble or particulate
- Decomposes to Ortho-P



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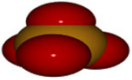

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Forms of Phosphorus

Orthophosphate

- Simple Phosphate, PO_4
- Soluble
- Phosphoric acid
- Conversion of organic and polyphosphate



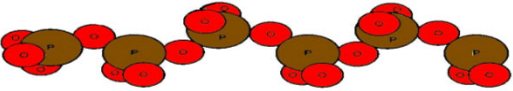




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Forms of Phosphorus

Polyphosphate (condensed phosphate)

- Chained molecules
- Soluble
- Detergents (no longer...!)
- Potable water treatment
- Decomposes to Ortho-P

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Forms of Phosphorus

FORM	REMOVAL PROCESS
<ul style="list-style-type: none"> • Organic-P 	<ul style="list-style-type: none"> • Converts to polyphosphate and orthophosphate forms; a small soluble portion is non-reactive (0.05 mg/l)
<ul style="list-style-type: none"> • Orthophosphate 	<ul style="list-style-type: none"> • Most abundant form; chemically reactive and consumed by biological growth
<ul style="list-style-type: none"> • Polyphosphates 	<ul style="list-style-type: none"> • Possibly reacts with metal salts; can be used for biological growth

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Forms of Phosphorus

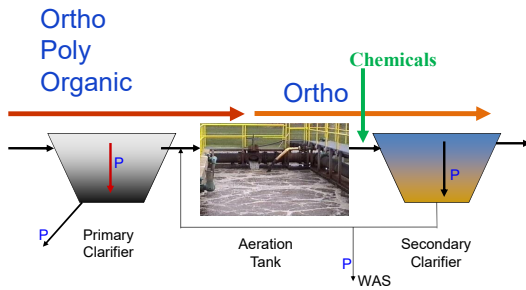
Total Phosphorus	Soluble Phosphorus	Ortho-P
		Poly-P
		Org-P NR Org-P
	Particulate Phosphorus	Colloidal Ortho-P
		Colloidal Poly-P
		Org-P

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Phosphorus Removal at WWTPs



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Phosphorus Removal at WWTPs

- Physical:
 - Sedimentation and filtration for particulate phosphorus
 - membrane technologies
- Chemical:
 - Co-precipitation
 - Chemical adsorption
- Biological
 - Assimilation
 - Enhanced biological phosphorus removal (EBPR)

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Background Uptake

- Physical removal of particulate organic phosphorus
- Conventional Biological Uptake
 - To satisfy biological needs
- Excess Biological uptake
 - Stress induced
 - Anaerobic zones
 - Release of phosphorus under anaerobic conditions
 - Uptake of phosphorus under aerobic conditions

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Phosphorus Removal Strategies

1. Source control: ban phosphates in detergents
2. Remove influent particulate P in primary clarifiers
3. Biologically convert soluble P to particulate forms
4. Chemically convert soluble P to particulate forms
5. Remove particulate P in final clarifiers and effluent filters
 - Particulate organic phosphorus
 - Biological (Phosphorus in microbial cells)
 - Chemical (Phosphate precipitates)

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Meeting Nutrient Discharge Limits Process Strategies

1. **Multiple barriers for TN removal**
 - Pre-anoxic zone (first stage denitrification)
 - Nitrification – aerobic zone
 - Post anoxic zone (second stage denitrification)
 - Denitrification filters (in lieu of post anoxic zone)
2. **Multiple barriers for TP removal**
 - Particulate P removal in primary clarifiers
 - Biological uptake (conventional, excess)
 - One (maybe two) chemical application points
 - Effluent filtration for particulate P removal

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Bans on Phosphorus in Detergents

- **By the mid-1970's, EPA** began advocating bans on detergent phosphates as practical and feasible approaches for reducing phosphorus loadings to the Great Lakes:
 - Bans on phosphates have met with consumer acceptance
 - Nitrilotriacetic acid and other phosphate substitutes have not proved to be a public health problem
 - Bans on phosphates reduce capital and operating costs (Chemical and sludge disposal) at WWTPs

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Bans on Phosphorus in Detergents

- States along the Great Lakes responded by:
 - Regulating phosphorus in detergents
 - Investing in more effective sewage treatment (e.g. phosphorus removal)
 - Developing and promoting best management practices for agriculture lands(e.g., minimizing surface runoff)

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Phosphate Bans in Detergents

In the mid-1980's, Maryland, Pennsylvania, Virginia, and the District of Columbia instituted bans on phosphates in laundry detergents



Nearly 25 years later, a second regional ban became effective on phosphates in automatic dishwasher detergents

Phosphate Bans in Detergents

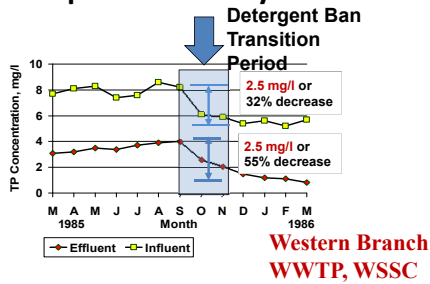
- Influent phosphorus concentrations to WWTPs were reduced more than 30% after the bans went into effect
- Effluent phosphorus concentrations from WWTPs were reduced more than 50%, after compensating for background uptake of phosphorus

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Ban on Laundry Detergent Phosphates in Maryland -1985



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Phosphorus Removal in Clarifiers

- Particulate organic phosphorus concentrations are likely high in “fresh” sewage
- Soluble phosphorus concentrations are likely high in “old” sewage
 - Conversion of particulate organic and condensed phosphorus forms to soluble phosphorus forms in the wastewater collection system

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Phosphorus Removal in Clarifiers

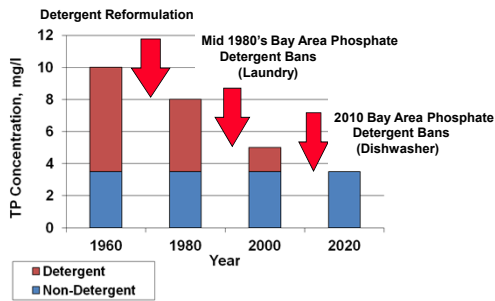
- Some phosphorus will be removed in the primary sedimentation tanks, e.g., 10 to 30%
- Removal in the primary clarifiers depends on influent phosphorus composition:
 - Particulate organic phosphorus
 - Particulate condensed phosphates

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WWTP – Influent TP Trend



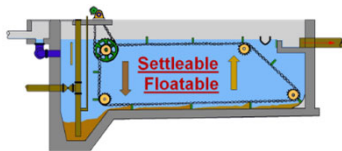
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Removal of Settleable Solids Provides Some Phosphorus Removal

Primary Sedimentation 10 - 30%



Biological Uptake

- Conventional Biological Uptake
 - To satisfy biological needs (2.0 to 3.0% by weight)
- Enhanced Biological uptake (5 to 7% by weight)
 - Stress induced
 - Release of phosphorus under anaerobic conditions
 - Uptake of phosphorus under aerobic conditions

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Biological Uptake

- **Assimilation** - Phosphorus removal from wastewater has long been achieved through incorporation of P as an essential element in the biomass

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Phosphorus Forms – Soluble versus Particulate

- Removal of soluble forms:
 - Biological:
 - Assimilation (In microbial cells)
 - Excess uptake – Enhanced Biological Phosphorus Removal (EBPR); A2O
 - Chemical precipitation and adsorption
 - Fe and Al salts
 - Lime

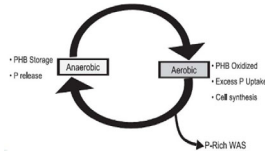
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Enhanced Biological P Removal (EBPR)

- Step 1: Anaerobic Phase
 - BOD removal
 - Phosphorus release
- Step 2: Aerobic Phase
 - Phosphorus uptake and creation of new PAOs
 - Phosphorus removal by sludge wasting



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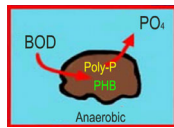
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Enhanced Biological P Removal (EBPR)

Anaerobic Conditions

PAO Take Up VFAs and Convert them to Polyhydroxybutyrate (PHB)



PAO Able to store soluble organics as Polyhydroxybutyrate (PHB)

Ortho-P is Released Into Solution

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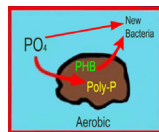
143

Enhanced Biological P Removal (EBPR)

Aerobic Conditions

Rapid Aerobic Metabolism of Stored Food (PHB) Producing New Cells

PO_4 Used in Cell Production
Excess Stored as Polyphosphate ("Luxury Uptake")

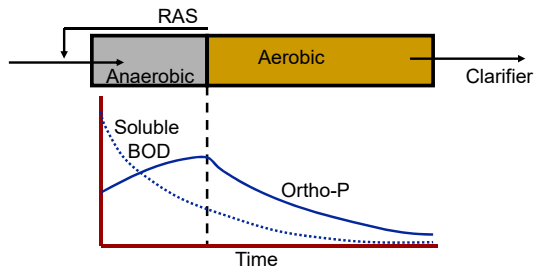


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Enhanced Biological P Removal (EBPR)



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Phosphorus Removal with Chemicals

Chemical Reactions – two mechanisms:

- **Co-precipitation** (Remove TP to ~ 0.5 mg/l)
 - $2Al + 3OH + PO_4 \rightarrow 2Al(OH)_3 \cdot PO_4 \downarrow$
- **Adsorption** (Remove TP < 0.5 mg/l to ~ 0.05)
 - $x (Al + 3OH) \rightarrow x (Al(OH)_3) \downarrow$
 - $x (Al(OH)_3) \downarrow + PO_4 \rightarrow x (Al(OH)_3) \cdot PO_4 \downarrow$
 - $x > 2$; more chemical required as PO_4 levels drop
- Both reactions form Metal (Al or Fe)-Phosphate-Hydroxide floc

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Co-Precipitation Iron Reactions

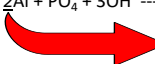
- $FeCl_3 + PO_4^{-3} \rightarrow FePO_4 + 3Cl^{-1}$
- $FeCl_3 + 3HCO_3^{-1} \rightarrow Fe(OH)_3 + 3CO_2 + 3Cl^{-1}$
- Simplified: $Fe + PO_4 \rightarrow FePO_4$
 $Fe + 3OH \rightarrow Fe(OH)_3$
- Combined:
 $2Fe + PO_4 + 3OH \rightarrow 2FePO_4(OH)_3 \text{ Complex} \downarrow$
 (Mole Ratio = 2.0)

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Co-Precipitation Aluminum Reactions

- $\text{Al}_2(\text{SO}_4)_3 \cdot 14\text{H}_2\text{O} + 2\text{PO}_4^{-3} \rightarrow 2\text{AlPO}_4 + 3\text{SO}_4^{-2} + 14\text{H}_2\text{O}$
- $\text{Al}_2(\text{SO}_4)_3 \cdot 14\text{H}_2\text{O} + 6\text{HCO}_3^{-1} \rightarrow 2\text{Al}(\text{OH})_3 + 6\text{CO}_2 + 14\text{H}_2$
- Simplified: $\text{Al} + \text{PO}_4 \rightarrow \text{AlPO}_4$
 $\text{Al} + 3\text{OH} \rightarrow \text{Al}(\text{OH})_3$
- Combined:
 $2\text{Al} + \text{PO}_4 + 3\text{OH} \rightarrow 2\text{AlPO}_4(\text{OH})_3 \text{ Complex}$ ↓
 (Mole Ratio = 2.0)

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Chemicals used for Phosphorus Precipitation

Chemical	Formula	Removal mechanism	Effect on pH
Ferric Chloride	FeCl_3 M.W. = 162.3	Metal hydroxides	Removes alkalinity
Aluminum Sulfate (Alum)	$\text{Al}_2(\text{SO}_4)_3 \cdot 14.3(\text{H}_2\text{O})$ M.W. = 599.4	Metal hydroxides	Removes alkalinity
Ferrous sulfate (pickle liquor)	Fe_2SO_4	Metal hydroxides	Removes alkalinity
Poly Aluminum Chloride	$\text{Al}_n\text{Cl}_{(3n-m)}(\text{OH})_m$ $\text{Al}_{12}\text{Cl}_{12}(\text{OH})_{24}$	Metal hydroxides	none
Lime	CaO , $\text{Ca}(\text{OH})_2$	Insoluble precipitate	Raises pH above 10

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Chemical Addition – Effects on pH

- Alum or iron salts will decrease alkalinity and pH, especially at higher dosages
- Lime raises pH
- PACl will not lower alkalinity or pH

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Chemical Addition Rates

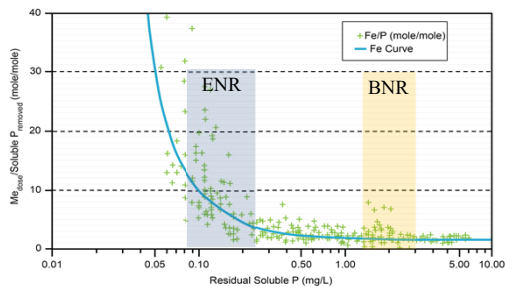
- Dependent on:
 - TP Discharge Limitations
 - Influx TP Loading
 - Biological P Removal Rates
 - Chemical to P Molar Ratios:
 - Al/Fe Salts, Range: 1.6- 2.1 to reach 0.5 mg/l P
 - > 3.0 to reach < 0.25 mg/l P
 - > 5.0 to reach < 0.2 mg/l P
 - >10 to reach < 0.15 mg/l P
 - Dependent on Alkalinity

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BNR and ENR

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Chemical Removal of Phosphorus



Data from the Blue Plains Advanced Wastewater Treatment Plant, Washington, D.C. and Lueddecke, C.; Hermanowicz, S.; Jenkins, D. (1987). Precipitation of Ferric Phosphate in Activated Sludge: A Chemical Model and Its Verification. Water Sci. Technol., 21, 325-338.

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Effluent Filtration Application

- Removes Residual Bio-Floc
- Removes Residual Chemical/Bio Floc
- Removes Residual Coagulation Particles in Phys-Chem Treatment

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Effluent Filtration Applications

- Gravity filters are needed to reduce effluent particulate phosphorus to less than 0.3 mg/L
- Membranes may be needed to reduce effluent particulate phosphorus to less than 0.1 mg/L

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Effluent Filtration Application

- Assuming that 2-3% of organic solids is P, then an effluent total suspended solids (TSS) of 10 mg/L represents 0.2-0.3 mg/L of effluent P.
- In plants with EBPR the P content is even higher
- Sand filtration or other method of TSS removal (e.g., membrane) is likely necessary for plants with low effluent TP permits

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TSS Removal Requirements

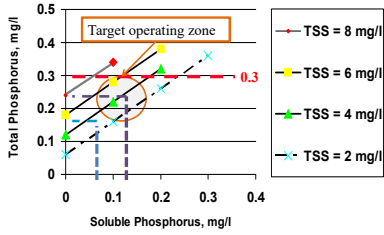
TP Limit, mg/L	Max TSS, mg/L
0.1	3.0
0.2	5.0
0.3	7.0
0.4	9.0
0.5	11

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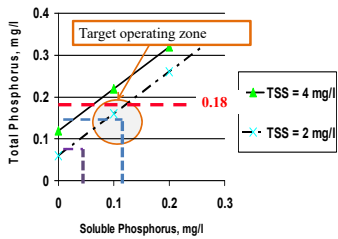
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Effluent TP versus Effluent TSS



Effluent TP versus Effluent TSS



What have you learned...

- What portion of TP is difficult to remove?

...non-reactive soluble Org-P

What have you learned...

- List three ways to remove phosphorus from wastewater?

...source control

...background/biological uptake

...chemical addition

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BNR and ENR

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What have you learned...

- The chemical dose for TP removal will depend on several factors; please list at least three...

...TP discharge limitations

...incoming TP loadings

...background/biological uptake rates of TP

...metal salt:TP mole ratio

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BNR and ENR

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What have you learned...

- List two common chemicals used to precipitate phosphorus from wastewater...

...FeCl₃

...Alum

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BNR and ENR

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BNR

Overview

March 2022 BNR and ENR 163

BNR Program

- To reduce total phosphorus concentrations, most WWTPs began adding chemicals like FeCl₃ or alum
- To reduce total nitrogen concentrations, most WWTPs initiated a capital improvement project to add “Pre” and/or “Post” anoxic zones to already existing nitrification processes for denitrification

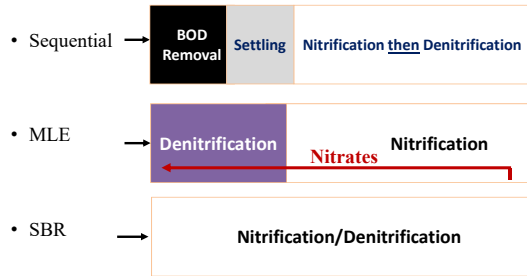
March 2022 BNR and ENR 164

Typical BNR Configurations

- **USEPA mode!** - Sequential BOD removal, Nitrification and Denitrification in separate basins
- **South Africa model (MLE)** – Modified Ludzack Ettinger process; Denitrification then Nitrification with nitrate recycle
- **SBRs** - Sequencing Batch Reactors; Nitrification then Denitrification in same basin; no nitrate recycle

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Typical BNR Configurations



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BNR and ENR

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BNR Processes

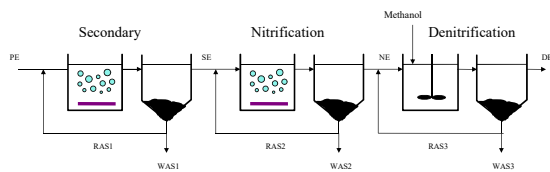
Process	Nitrogen	Phosphorus	Comments
MLE	Good	None	- Moderate basin volume
Enhanced MLE (Bardenpho)	Excellent	None	- Large basin volume - Need for methanol
Step Feed	Good	None	- No nitrate recycle
SBR	Moderate	Inconsistent	- No nitrate recycle
A ² O	Good	Good	- Moderate basin volume - Sensitive to DO in return
Modified UCT	Good	Excellent	- Separate anoxic zone for RAS - Several nitrate recycle streams - Increased complexity
5-stage Bardenpho	Excellent	Good	- Larger reactor volume - Need for methanol
Oxidation Ditch	Excellent	Good	- Long HRT and SRT - Tight DO controls necessary

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EPA "Model" for TN Removal

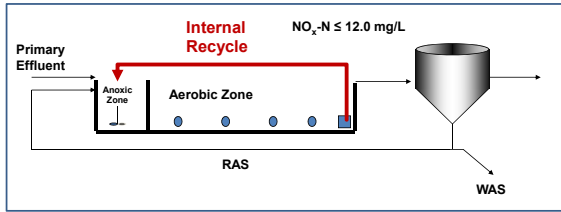


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MLE with Internal Recycle

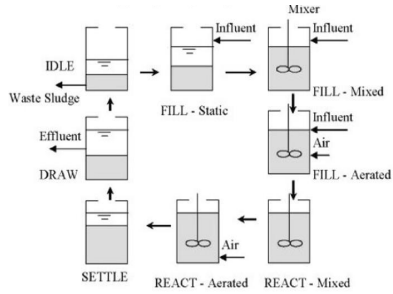


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Sequencing Batch Reactor

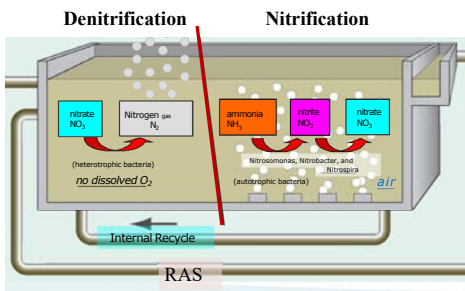


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Biological Nitrogen Removal



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BNR and ENR

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BNR Program

- BNR Programs in Bay watershed states began removing nutrients in 1985
- For WWTPs greater than 0.5 mgd:
 - 95% of wastewater discharged into the Bay
 - Grant funding available for WWTP upgrades
- WWTP discharge goals:
 - Reduce TP from ~ 6 mg/l to < 3.0 mg/l
 - Reduce TN from ~ 20 mg/l to < 8.0 mg/l

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BNR and ENR

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Biological Nutrient Removal (BNR)

- BNR converts/removes Nitrogen (primarily ammonia – NH_3) in wastewater to nitrite (NO_2), nitrate (NO_3), and ultimately nitrogen gas (N_2).
- BNR is a two-step process:
 - Step 1: Nitrification
 - Step 2: Denitrification

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BNR and ENR

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BNR

- Removes most nitrogen (TN) and phosphorus (TP) from wastewater
- BNR processes use microorganisms under different environmental conditions:
 - Anaerobic (w/o O_2 and $\text{NO}_3\text{-N}$)
 - Anoxic (w/o O_2)
 - Aerobic or oxidic (with O_2)

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BNR and ENR

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BNR Stages

- Anaerobic stage - No oxygen nor $\text{NO}_3\text{-N}$; Phosphorus is released; enhances greater TP uptake in the aerobic stage
- Anoxic stage - No oxygen; $\text{NO}_3\text{-N}$ is converted to N_2 gas (Denitrification)
- Aerobic stage - Plenty of oxygen; $\text{NH}_3\text{-N}$ is converted to $\text{NO}_3\text{-N}$ (Nitrification)

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Milestones

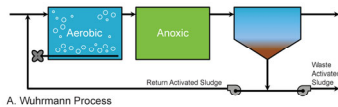
- 1954 Wuhrman proposes 2-stage, aerobic - anoxic process
- 1962 Ludzack and Ettinger proposes 2-stage, anoxic - aerobic process
- 1973 Barnard in South Africa develops the Modified Ludzack-Ettinger process

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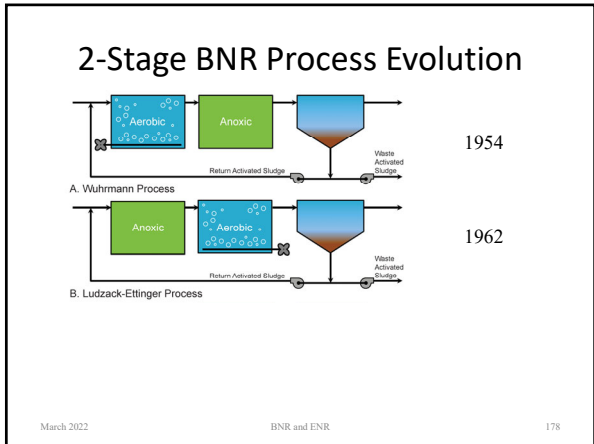
2-Stage BNR Process Evolution

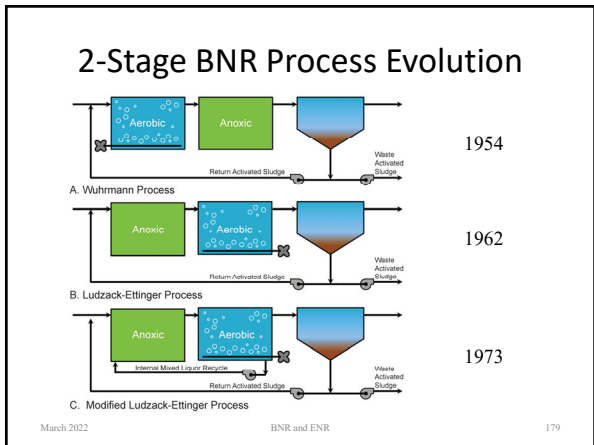


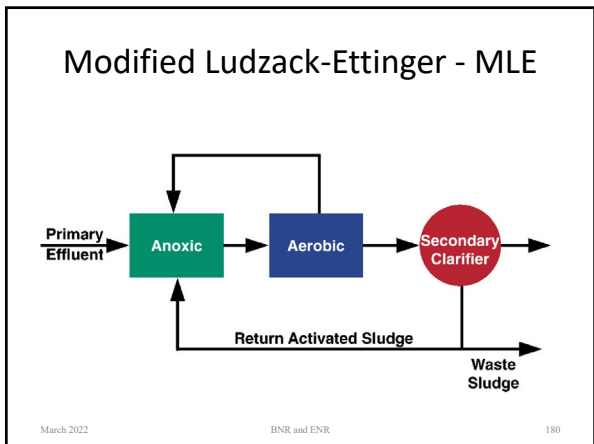
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Milestone

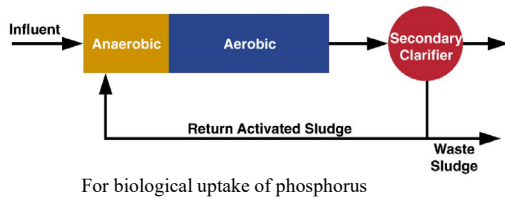
- 1976 Specter patents A/O® and A²/O® processes

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AO

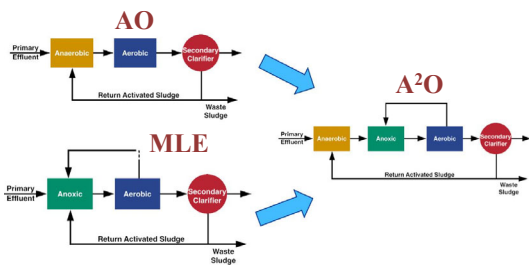


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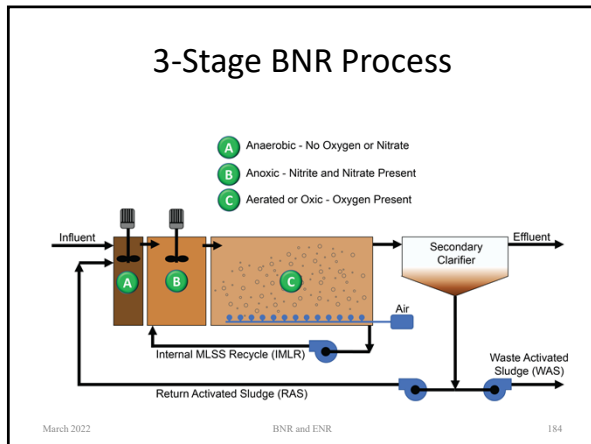
AO plus MLE = A²O

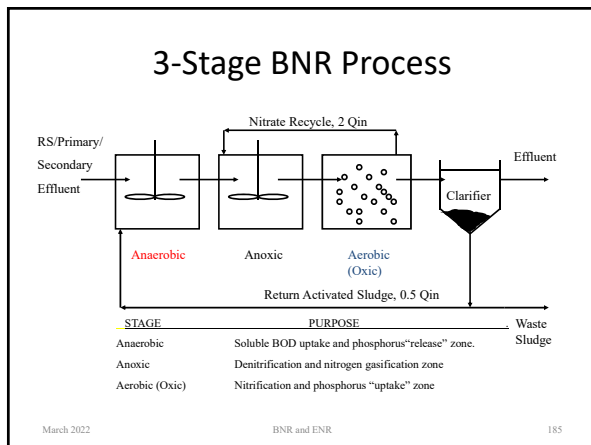


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BNR and ENR

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Historical View of BNR

- Recent efforts for nutrient removal for WWTPs with limited space for expansion has led to:
 - Membrane reactors
 - Side-stream treatment for phosphorus removal:
 - Struvite precipitation
 - Side-stream treatment for ammonia removal:
 - ANAMMOX

March 2022 BNR and ENR 186

What have you learned...

- What was the regulatory “drivers” for BNR programs in Chesapeake Bay states?

...EPA’s Chesapeake Bay Program (1983)
...1987 Chesapeake Bay Agreement

March 2022 BNR and ENR 187

What have you learned...

- What was the regulatory “driver” for ENR programs in Chesapeake Bay states?

...2000 Chesapeake Bay Agreement

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What have you learned...

- When did Dr. Barnard develop the modified Ludzack- Ettinger (MLE) process? Why is this significant?

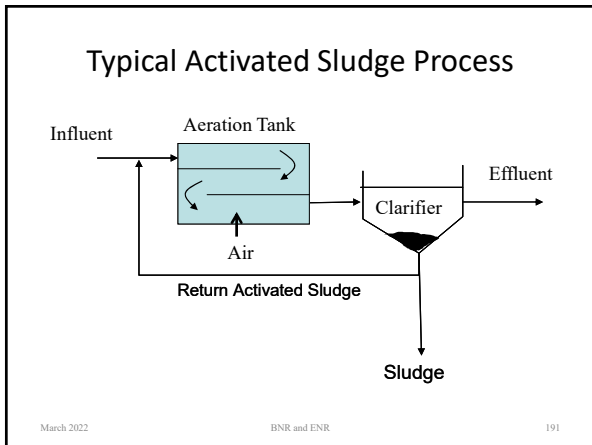
...1973 (added internal nitrate recycle)
...The MLE concept is the standard for wastewater processes

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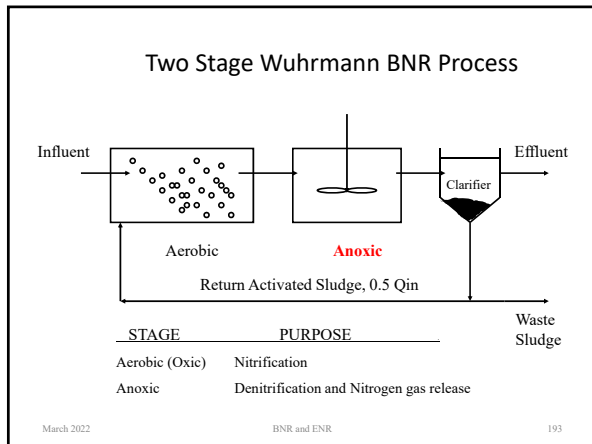
BNR

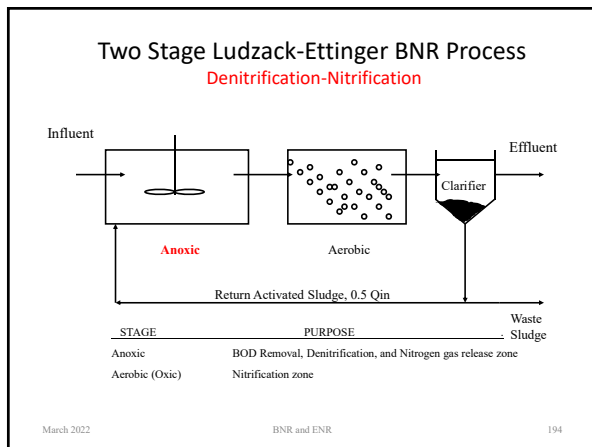
Process Details

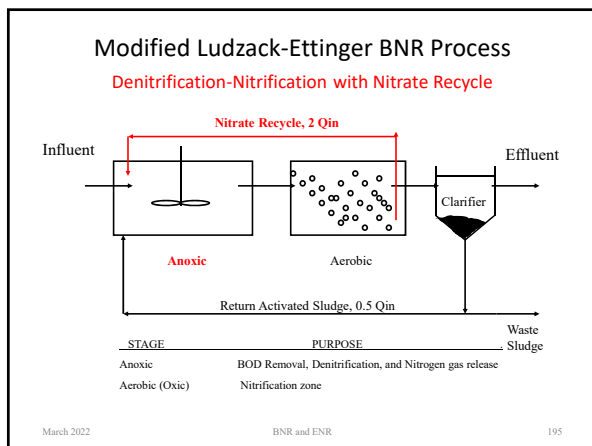
March 2022 BNR and ENR 190



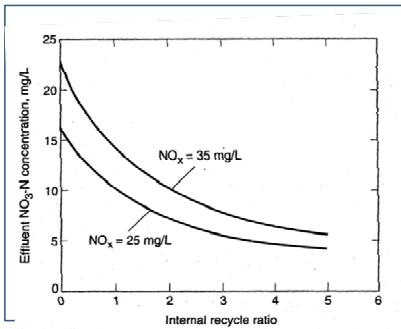
- ### BNR Processes
- Anaerobic-aerobic (AO)
 - Modified Ludzack-Ettinger (MLE)
 - Anoxic-aerobic
 - Anaerobic-anoxic-oxic (A²O and UCT)
 - Step feed
 - Oxidation ditch
- March 2022 BNR and ENR 192







Impact of Internal Recycle on Effluent TN

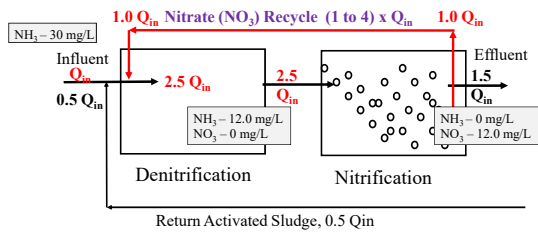


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BNR and ENR

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TN Removal – Example 1



Return Activated Sludge, $0.5 Q_{in}$

Assume all NO_3 returned to Denitrification is converted to N_2

Assume all NH_3 -N is converted to NO_3 -N in Nitrification.

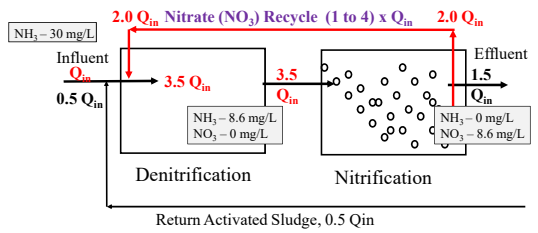
What is the NH_3 -N concentration in Denitrification? $NH_3-N = \frac{30 \text{ mg/L} \times 12.0 \text{ mg/L}}{2.5/1}$

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BNR and ENR

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TN Removal – Example 2



Return Activated Sludge, $0.5 Q_{in}$

Assume all NO_3 returned to Denitrification is converted to N_2

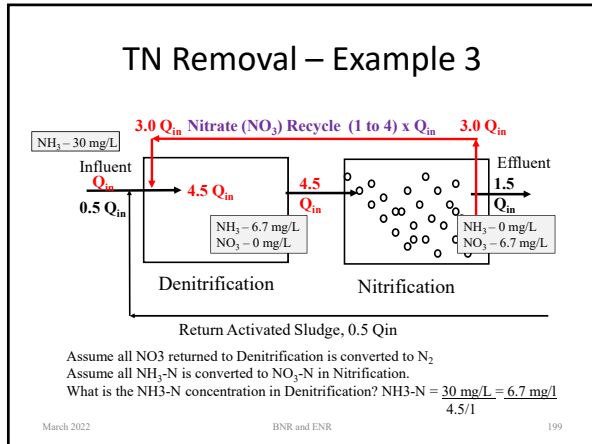
Assume all NH_3 -N is converted to NO_3 -N in Nitrification.

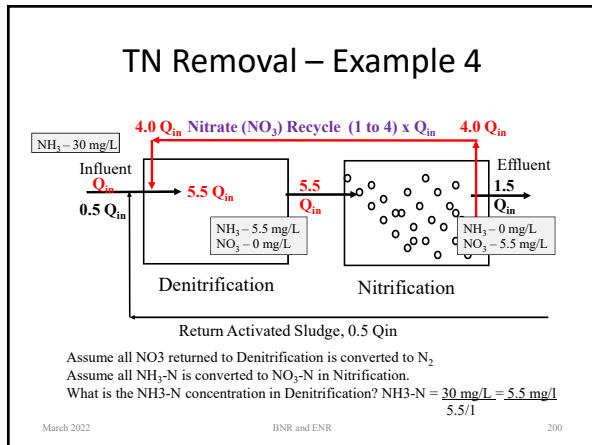
What is the NH_3 -N concentration in Denitrification? $NH_3-N = \frac{30 \text{ mg/L} \times 8.6 \text{ mg/L}}{3.5/1}$

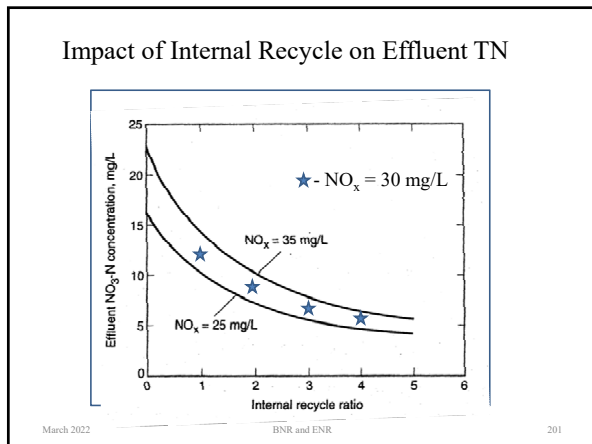
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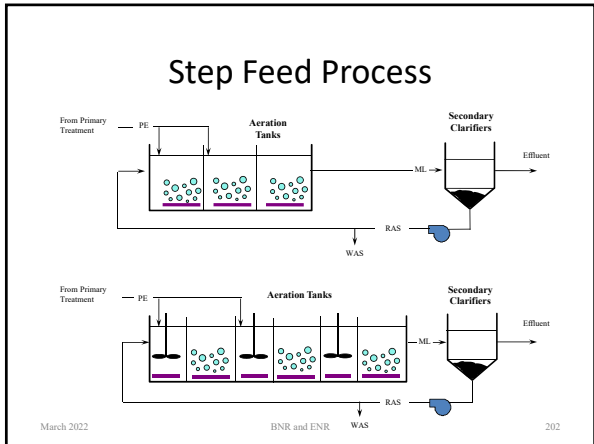
BNR and ENR

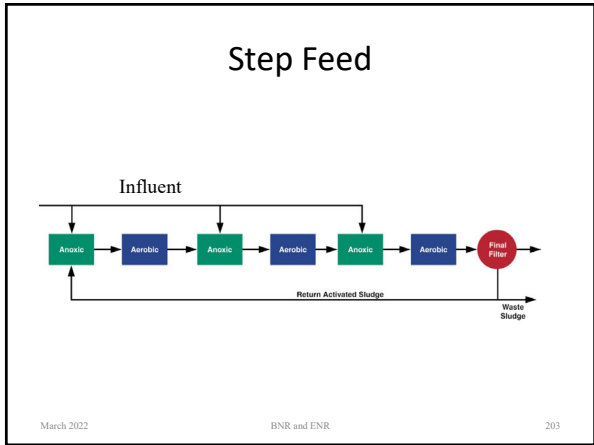
198

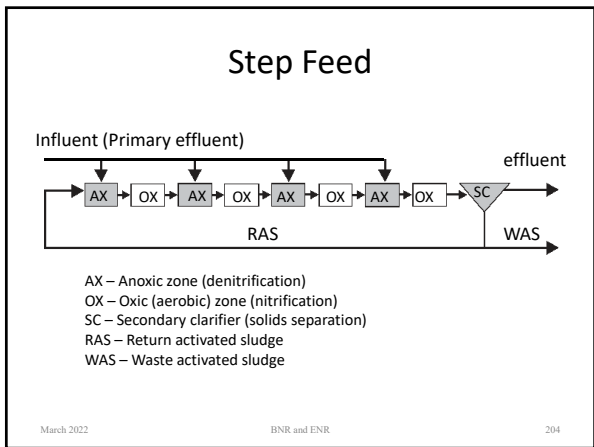


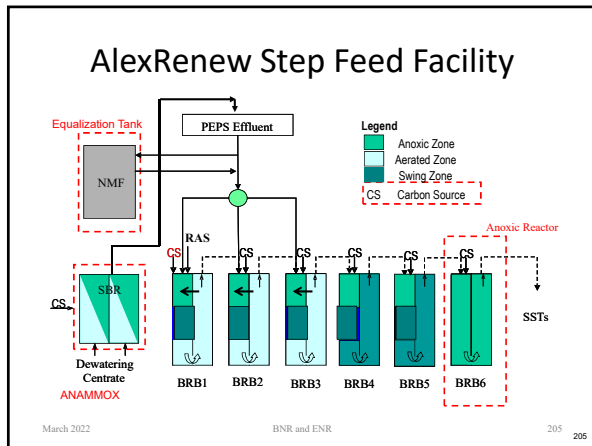


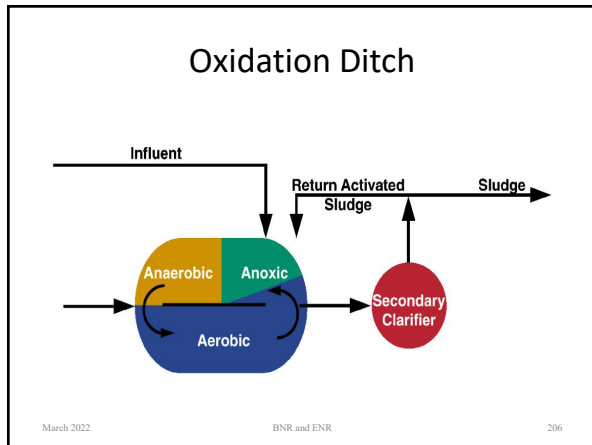


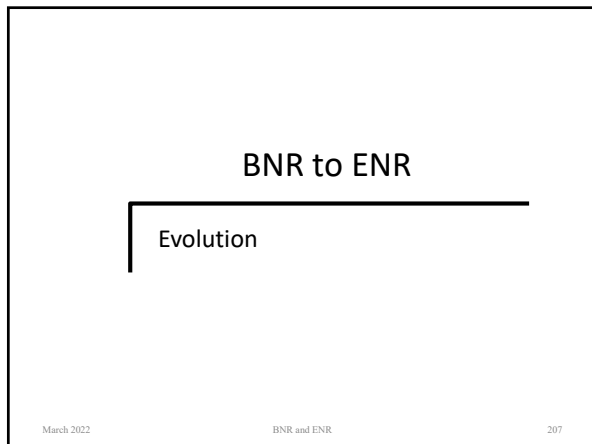




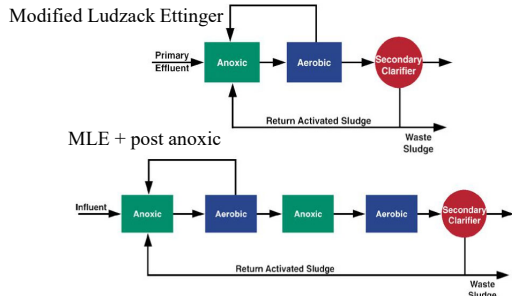








Example of BNR to ENR



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BNR and ENR

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Milestones

- 1968 Barth proposes 3-sludge, activated sludge process for nutrient removal
- 1975 Barnard patents Bardenpho® process
- 1980 University of Cape Town (UCT) process developed

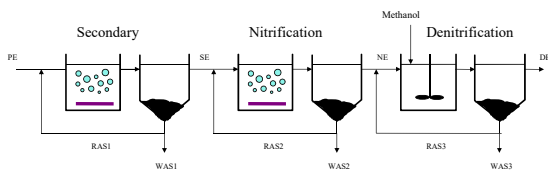
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BNR and ENR

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Three Stage System for BOD and Nitrogen Removal

Post Denitrification w/Methanol



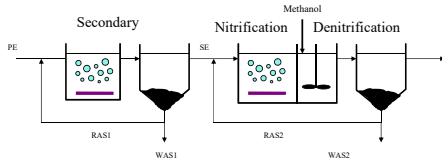
Example: Western Branch WWTP, WSSC 30 MGD

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Two Sludge System for BOD and Nitrogen Removal



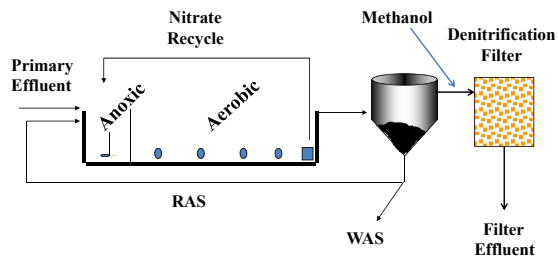
Example: Blue Plains, DC Water 370 MGD

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BNR and ENR

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MLE With Denitrification Filter



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BNR to ENR

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What have you learned...

- What process is needed to go from BNR to ENR?

...a post denitrification process

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BNR and ENR

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What have you learned...

- List three BNR/ENR processes that remove TN to less than 5.0 mg/L...
 - ...MLE
 - ...Enhanced MLE
 - ...step feed
 - ...UCT
 - ...Oxidation ditch

March 2022 BNR and ENR 214

What have you learned...

- The amount of TN removal in BNR processes depends primarily on the...
 - ...Nitrate recycle rate from nitrification to denitrification
 - ...amount of nitrates returned to the denitrification process

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ENR

└── Overview

March 2022 BNR and ENR 216

ENR Program

- To further reduce total phosphorus concentrations, most WWTPs began adding increased quantities of chemicals
- To further reduce total nitrogen concentrations, most WWTPs initiated a capital improvement project to add "Post" anoxic zones to already existing BNR facilities

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BNR and ENR

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ENR Program

- ENR Program began in 2000
- For WWTPs greater than 0.5 mgd
 - 95% of wastewater discharged into the Chesapeake Bay
 - Grant funding available for upgrades
- WWTP discharge reduction goals:
 - Reduce TP from < 3.0 mg/l to < 0.3 mg/l
 - Reduce TN from < 8.0 mg/l to < 3.0 mg/l

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BNR and ENR

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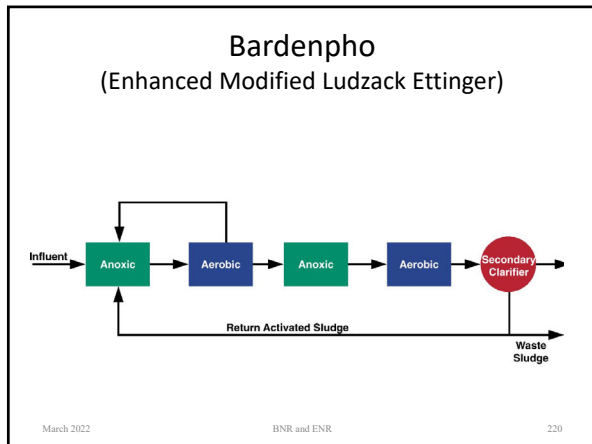
Enhanced Nutrient Removal

- Over the past two decades, BNR facilities have been upgraded to improve nitrogen removal efficiencies:
 - Post anoxic zones for denitrification
 - Mixed Bed Bio-reactors (MBBR)
 - Fixed film biological filters for nitrification
 - Tertiary denitrification filters

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BNR and ENR

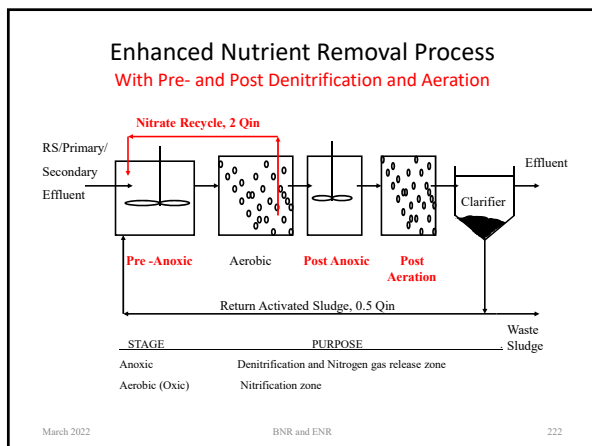
219



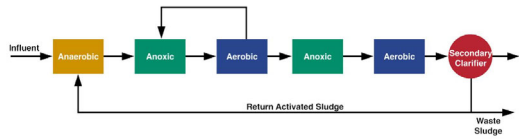
Enhanced Nutrient Removal

- For WWTPs to upgrade from BNR to ENR, and satisfy new LOT requirements for nitrogen removal, an additional post-denitrification stage is required; for example:
 - MLE + post anoxic
 - MLE + MBBR
 - MLE + Denit Filter
 - Step feed + post anoxic
 - Step feed + MBBR
 - Step feed + Denit Filter

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Modified Bardenpho

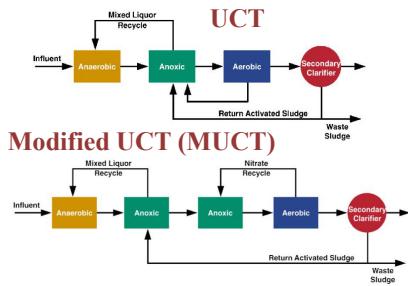


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BNR and ENR

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UCT Processes



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BNR and ENR

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Denitrification

Note: (Almost) all nitrates entering anoxic zones should be denitrified

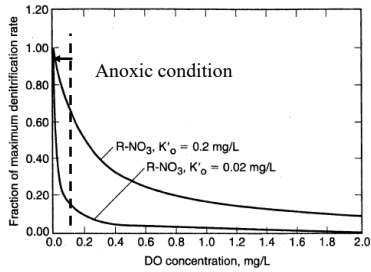
The effluent "goal" $\text{NO}_3\text{-N}$ concentration from the last anoxic zone should be between 0 and 0.5 mg/L.

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BNR and ENR

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Reduction in rate of Denite as a function of D.O.
(K'o is oxygen inhibition constant)



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Carbon for Denitrification

- Influent WW Carbon
 - Utilized in anoxic zones
 - Limited carbon available for secondary anoxic zones
- Supplemental Carbon
 - Methanol typically used
 - But requires methylotrophic population!
 - Alternatives to methanol – glycerin, sugars, and proprietary products

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BNR and ENR

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Carbon for Denitrification

- If using methanol – may not have adequate methylotrophic population
 - Need well controlled anoxic volume
 - Methylotrophs require acclimation time
 - Methylotrophs are believed to be more sensitive to temperature
- Methanol is typically more sensitive to pH and may not be effective in very cold weather
 - Change carbon source – ethanol or glycerin
- Denitrification batch tests
 - Specific denitrification rates (SDNRs) – different carbon sources

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BNR and ENR

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Other Carbon Sources

- Alcohols
 - Methanol
 - Ethanol
- Glycerol/glycerin – (Biodiesel by-products)
- Acetates - (Acetic acid, sodium acetate)
- Carbohydrates - (Sucrose, sugar water, corn syrup)
- MicroC™ – (Carbohydrate, glycerin, alcohol based blends)

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Denitrification Problems

Possible Causes	Solution
Not enough nitrates being returned to anoxic zone	Increase nitrate recycle pump speed
Not enough BOD entering anoxic zone	- Bypass primary clarifiers, or - Add supplemental carbon (for example, methanol) to anoxic zone
BOD entering the anoxic zone breaks down too slowly	Add readily available carbon source such as methanol to anoxic zone or increase the anoxic zone hydraulic retention time
High DO in the anoxic zone	Try to limit backmixing of air from the aerobic zones or decreasing the DO in the AT influent. Decrease nitrate recycle rate if necessary.

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BNR and ENR

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What have you learned...

- List four distinct forms of nitrogen in wastewater making up total nitrogen (TN)...

$\left. \begin{array}{l} \dots \text{Org-N} \\ \dots \text{NH}_3\text{-N} \end{array} \right\} \text{TKN, un-oxidized nitrogen}$
 $\left. \begin{array}{l} \dots \text{NO}_2\text{-N} \\ \dots \text{NO}_3\text{-N} \end{array} \right\} \text{Oxidized nitrogen}$

$$\dots \text{TN} = \text{Org N} + \text{NH}_3 + \text{NO}_2\text{-N} + \text{NO}_3\text{-N}$$

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What have you learned...

- What portion of TN is difficult to remove?

...non-reactive soluble Org-N

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What have you learned...

- What are the two processes needed to remove TN?

...Nitrification
...Denitrification

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What have you learned...

- Below average wastewater temperatures (increase or decrease) the growth rate of nitrifiers...

...decrease

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What have you learned...

- List three factors key to nitrification...

...Maintain target solids residence times (SRT) or mean cell residence times (MCRT)

...Maintain target DO levels – 2 to 4 mg/l

...Maintain target alkalinity levels - > 70 mg/l CaCO₃

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What have you learned...

- What substance needs to be absent to assure denitrification?

...Dissolved Oxygen

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BNR and ENR

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What have you learned...

- Which process is key to TN removal, nitrification or denitrification?

...Nitrification

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Fixed Film Processes

Nutrient Removal

March 2022 BNR and ENR 238

Fixed Film Processes

- cBOD Removal
 - TF – Tricking Filters
 - RBC – Rotating Biological Contactor
- Nitrification
 - BAF – Biological Aerated Filter
 - IFAS – Integrated Fixed-Film Activated Sludge
 - MBBR – Moving Bed Biofilm Reactor
- Denitrification
 - Denit Filter
 - Down flow
 - Up flow

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Fixed Film Processes

cBOD Removal	Nitrification	Denitrification
<ul style="list-style-type: none"> – TF – RBC – BAF 	<ul style="list-style-type: none"> – TF & RBCs – BAF – IFAS – MBBR 	<ul style="list-style-type: none"> – Denit Filters – MBBR (w/o O₂) – BAF (w/o O₂)

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Fixed Film Processes

What can fixed film (a.k.a. attached growth) processes do?

1. Remove Nutrients

- Phosphorus
- Nitrogen

2. Remove BOD:

- Dissolved organic solids

3. Remove TSS:

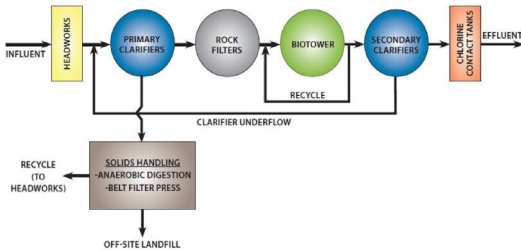
- Suspended particulate solids
- Suspended organic solids

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Process Configuration Nitrification

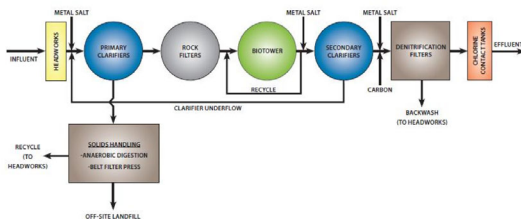


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Process Configuration ENR with Denitrification Filters

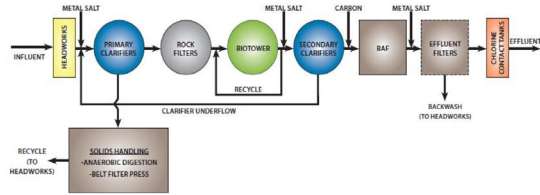


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Process Configuration ENR with Denit-BAF and Effluent Filters

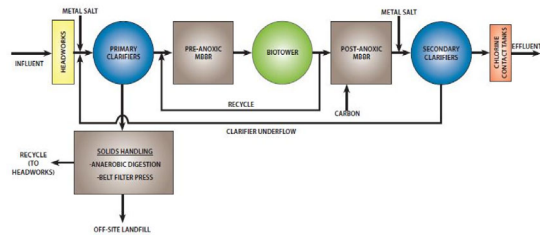


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Process Configuration ENR with Pre- and Post-anoxic MBBR



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Fixed Film Nitrification

IFAS and MBBR

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Why Use An IFAS Process ?

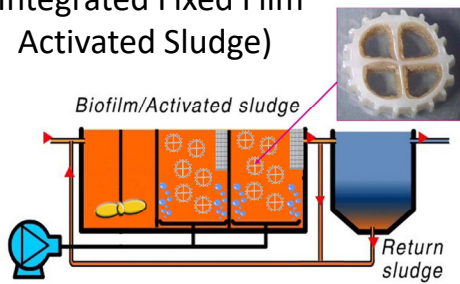
- Increase capacity without more tanks
- Achieve nitrogen removal in tank, which could not otherwise totally nitrify and denitrify

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IFAS (Integrated Fixed Film Activated Sludge)

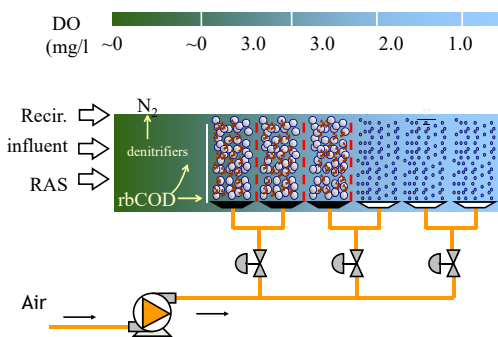


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IFAS LAYOUT



IFAS in Nutrient Removal

Typically an upgrade to implement BNR or increase Nitrification capacity at existing plants.

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Benefits of IFAS Processes

- Increase total solids inventory without increasing solids loading to clarifier
- Minimize effects of solids washout under high hydraulic loadings
- Avoid cost of construction of new tanks
- Decrease required recycle rates

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Plant Configurations

1A. Activated Sludge

1B. IFAS – fixed bed
Eg: Ringlace, Bioweb (cord)

1C. IFAS – Moving Bed
Eg: Linpor, Captor (sponge)
Kaldnes, Hydroxyl, Bioportz (plastic)

1D. MBBR – Moving Bed Biofilm Reactor
Kaldnes (plastic)

From 1A to 1D
Clarifier size requirements decrease; Operating MLSS HRT requirements decrease; Biofilm surface area increases

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Types of IFAS Systems

Fixed

Free

Rope

Plastic

Sponge

Plastic

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Free Floating Media - Plastic

Hydroxyl

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Free Floating Media - Sponge

Lotepro – Linpor Process


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Plastic Media (Kaldnes)


		K1	K2	K3	Model O	Biofilm Chip
Length	(mm)	7.2	15	9	50	2
Diameter	(mm)	9.1	15	25	60	47
Specific Surface Area	(m ² /m ³)	500	350	480	94.5	1,200




K1



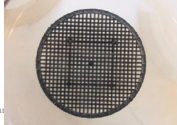
K2



K3



Model O



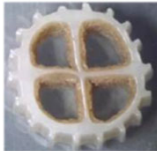




Biofilm Chip

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Integrated Fixed Film Activated Sludge System

- Media held in Aeration Basins to provide attached growth for Nitrifying biomass
- Typical Floating and Fixed IFAS Media
 - Kaldnes (plastic)
 - Linpor (sponge)
 - Ringlace (cord)

BNR and ENR 257

What have you learned...

- What does the acronym IFAS stand for?

...Integrated Fixed Film Activated Sludge

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What have you learned...

- What does the acronym MBBR stand for?

...Moving Bed Bioreactor

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What have you learned...

- Why are IFAS systems used?

...to increase nitrification capacity without building more tanks

...to increase total solids inventory

...to minimize effects of solids washout under high hydraulic loadings

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Fixed Film Nitrification

Biological Aerated Filter - BAF

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Submerged BAFs



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Submerged BAFs

- Biofor® - Up flow filter (Infilco Degremont)
 - Aerated, fixed bed
 - Dense granular clay media
 - “Sinking” media; 3 mm diameter for nitrification
- Biostyr® - Up flow filter (Veolia Water/Kruger)
 - Aerated, packed bed
 - Media less dense than water held in place by a screen
 - “Floating” media; 3 mm diameter for nitrification

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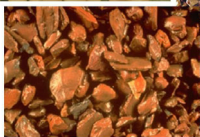
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BAF Media



Fine material
- Good filtration
- Large, specific surface area



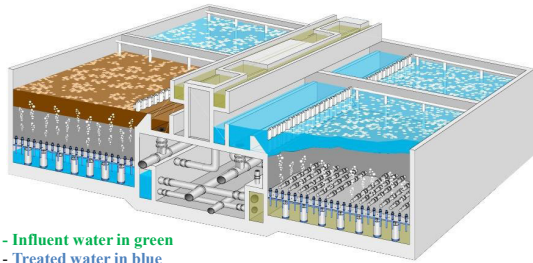
Coarse material
- Less clogging

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BIOFOR® Process View with One Cell in Backwash



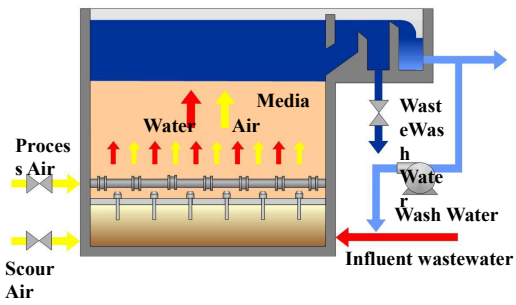
- Influent water in green
- Treated water in blue
- Process air and air scour bubbles in white

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BIOFOR® Sequences

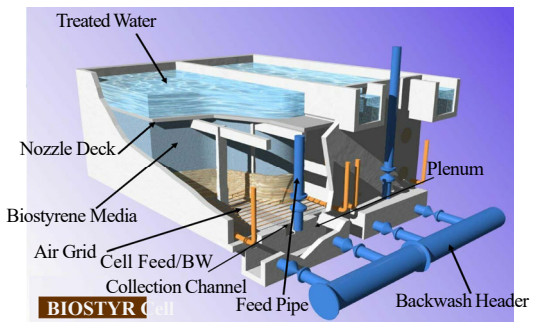


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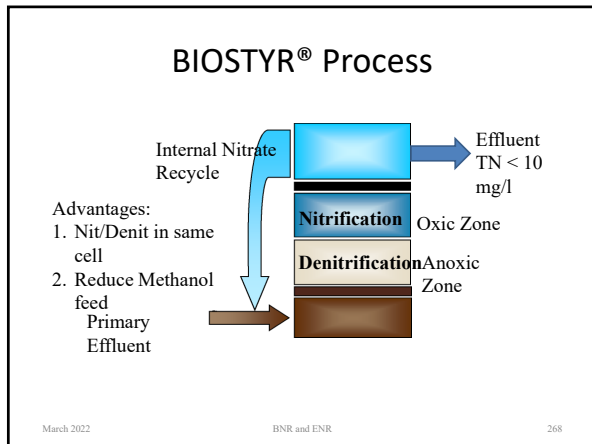
BIOSTYR® Process

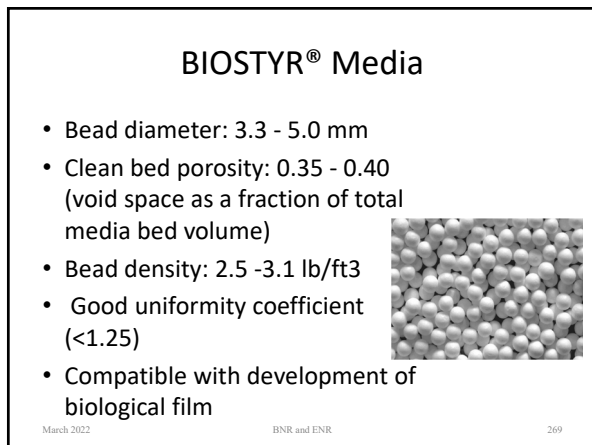


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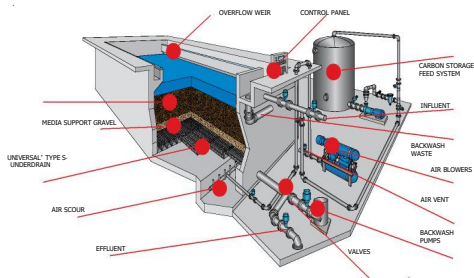
The TETRA® Denite® system from Severn Trent Services removes nitrate-nitrogen and suspended solids in a single step. It is used as a tertiary process on effluents from wastewater treatment plants. TETRA was recently awarded a contract to supply their TETRA® Denite® system for use at the Baltimore City Patapsco WWTP.

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Leopold® elimi-NITE® Denitrification System



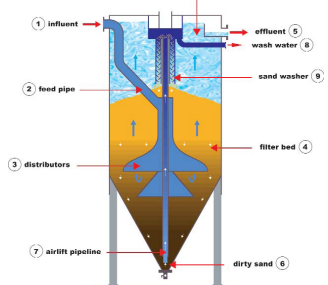
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Up Flow Denit Filters

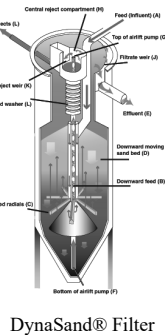
Astrasand® Filter



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DynaSand® Filter


Solids Handling Side Streams

Nutrient Removal Systems

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What are Sidestreams

- Any process flow resulting from the treatment of biosolids that flows back into the liquid treatment train
- Examples:
 - Gravity Thickener Overflow
 - Gravity Belt Thickener filtrate
 - Belt Filter Press filtrate
 - Centrate
 - Digester supernatant



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Common Side-stream Treatment Alternatives for N & P Removal

Biological Treatment

1. Bio-augmentation of nitrification/denitrification
 - In-Nitri
 - BABE process
 - New York AT3
 - MAUREEN process
2. Nitrogen removal by nitration and denitration
 - SHARON process
3. Nitrogen removal by de-ammonification
 - ANAMMOX process
 - DEMON process
 - CANON process

Physio-Chemical Treatment

4. Ammonia Stripping
 - Hot air
 - Steam
5. Ion exchange in selective resins
 - ARP process
6. Struvite (MAP) precipitation
 - OSTARA process
 - PhosPaq process
 - Multifarm Harvest
7. Breakpoint Chlorination

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Why consider side-stream treatment?

- Concentrated nutrient load
- Usually economical when sidestreams contribute:
 - $\geq 15\%$ of the influent TN
 - $\geq 20\%$ and TP load
 - Typ. of plants with significant biological processes in the solids train (i.e., anaerobic digestion)
- Can often reuse existing infrastructure to reduce costs
- However, sidestream treatment is not economical in many cases

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Nitrogen Removal

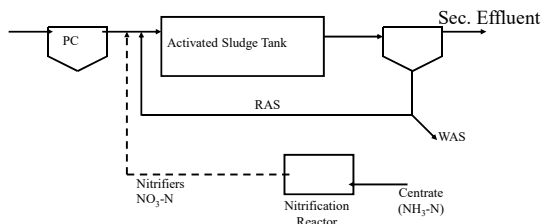
- Bioaugmentation
 - In-Nitri
 - BABE
 - NYC AT-3
 - MAUREEN
- Nitritation/Denitritation
 - SHARON
 - STRASS
- Nitritation/Deammonification
 - ANAMMOX
 - DEMON
 - CLEAR Green
 - ANITA Mox

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InNitri Process was the first bioaugmentation scheme

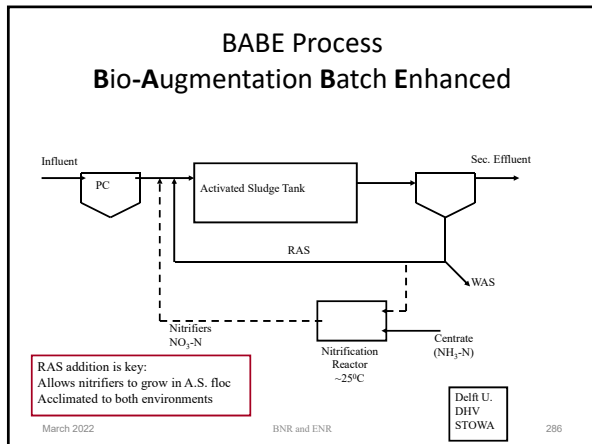


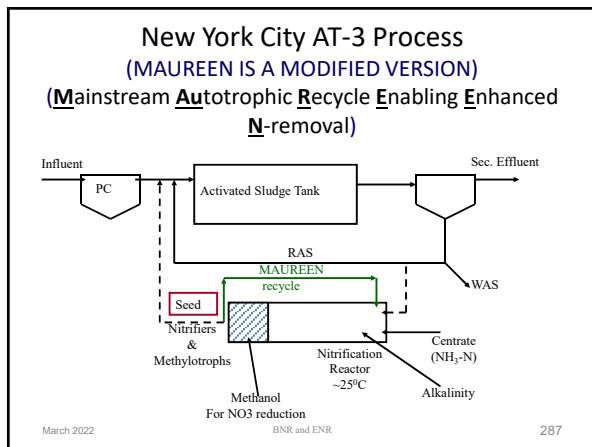
Expected benefit not fully realized
Temperature change
Poor capture of recycle stream nitrifiers
Predation
Change in total dissolved solids content – osmotic pressure

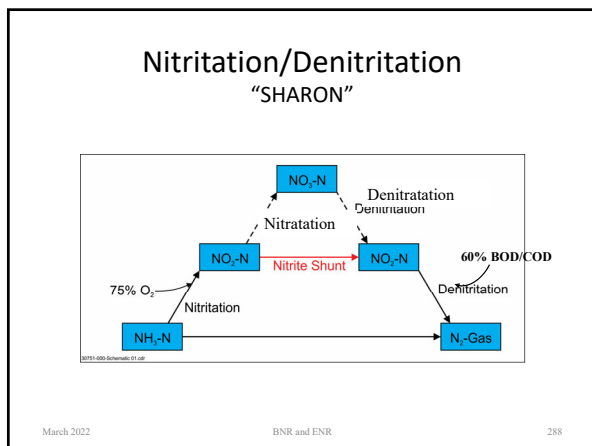
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Key Drivers for Side-stream Phosphorus Removal Systems

- High side-stream contribution of phosphorus affecting biological phosphorus removal, usually coupled with low TP limits (< 0.3 mg/L)
- Land application program with limitations on agronomic rates of N or P application
- Severe struvite problems

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BioMag™
The Next Generation of Biological Treatment

Cambridge Water Technology's BioMag Process® uses Magnetite (Fe_3O_4) as a flocculation aid to improve settling characteristics of activated sludge. With a specific gravity of 5.2 and a strong affinity for biological solids, magnetite can significantly decrease SVI's and increase MLSS settling rates to handle higher flows. Enhanced nutrient removals, especially phosphorus, are possible.

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Side Stream Phosphorus Treatment: Two Alternatives

1. Coagulant-aided phosphorus precipitation
 - Forms aluminum phosphate and aluminum hydroxide
 - Non-proprietary
2. Struvite formation
 - Forms struvite
 - Proprietary
 - Ostara & Multifarm Harvest

Of these two options, only struvite has been identified as a fertilizer additive with market value

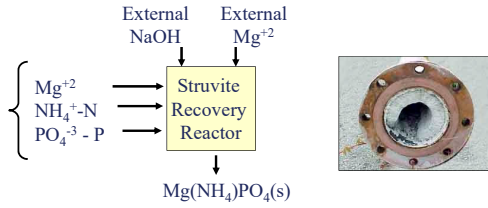
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How Struvite Precipitation Works

- Struvite precipitation
 - N:P ratio in struvite = 0.45 lbs N required per lb P removed
 - N:P ratio in filtrate ~ 2.4-2.6, ammonia in excess



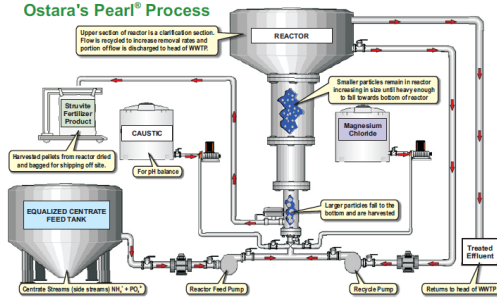
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Schematic of Ostara Process

Ostara's Pearl® Process



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Crystal Green™ fertilizer

- Fertilizer for parks and golf courses
- Specialized product
- Green attributes
 - Slow release fertilizer
 - Produced with minimal greenhouse gas emissions
 - Renewable source
 - Reduces mining of phosphorus for use in commercial fertilizers



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Multiform Harvest

- Simple process to operate – struvite processed offsite
- Filtrate passes through once

3 ENR 298

Ostara vs. Multiform product

Ostara Pearl	Multiform Harvest
--------------	-------------------

$$\text{Mg}^{+2} + \text{NH}_4^+ + \text{PO}_4^{-3} + 6\text{H}_2\text{O} \rightarrow \text{MgNH}_4\text{PO}_4 \cdot 6\text{H}_2\text{O} \text{ (struvite)}$$

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Summary

Helpful Hints - Final Comments

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Helpful Hints

- Consider multiple “barriers” for TP and TN removal, e.g. post anoxic zone
- Nitrification is “Key” to the success of BNR/ENR processes when removing TN
- Nitrify completely – $\text{NH}_3 < 0.1 \text{ mg/L}$; no NO_2^-
- Maintain $< 0.2 \text{ mg/L}$ D.O. in denitrification process to maximize denitrification rate
- Allow for excess chemical addition (5 – 7 mole ratio) to meet TP levels $< 0.18 \text{ mg/?}$

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Final Comments

- Many possible causes for poor nutrient removal performance
- Important to determine cause and act quickly to maintain chemical and biological processes
- Basic troubleshooting approaches are universal.
- Sidestream treatment can significantly reduce TP and TN loadings to mainstream process.

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Questions?



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Thank You

Maryland Center for Environmental
Training
College of Southern Maryland
La Plata, MD

"Anyone who can solve the
problems of water will be
worthy of two Nobel prizes –
one for peace and one for
science."

- John F. Kennedy



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